

**Pinnacle Renewable Energy Inc
Smithers Pellet Limited Partnership**

**Total Particulate & Condensable Organics
February 13, 2025
Smithers, B.C.
Permit 06099**

Our Job Number: ME2425-152

Report Author: Matt McCall
McCall Environmental



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February 28, 2025

Smithers Pellet Limited Partnership
1723 Dahlie Rd
PO Box 699
Smithers BC
V0J 2N0

Attention: Joel Martens/Wayne Kooy
RE: Air Emission Testing Feb 13, 2025
RA-6099, ME2425-152

As requested our firm provided a series of air emission tests at your facility in Smithers, B.C. The purpose of these tests was to satisfy testing requirements as stated in your permit RA-6099.

Testing Parameters

- Total Particulate and Condensable Organics (4 Sources)
 - o State of Oregon Method

Key Personnel

- Report Generation: Matt McCall 250-542-5118
- Sr Field Tech: Dave Brandle, Dan Lawrence 250-301-5712
- Plant Personnel: Joel Martens 250-847-1431

All stacks have been examined for cyclonic flow and determined to be tested as laminar in nature.

Test results are summarized immediately following this cover letter.

Lab analysis for condensable organic fractions was carried out by Element Labs in Surrey, B.C. A copy of their report is included in the Appendix of this report.

If you have any questions or concerns please don't hesitate to contact us at your earliest convenience.

Sincerely,

MCCALL ENVIRONMENTAL

Matt McCall

Summary of Test Results

Parameter	Average of Triplicate Tests				Avg/ Comb	Permit	Prev Test
	Stack 1	Stack2	Stack 3	Stack 4			21- Nov-24
Test Date	13-Feb-25	13-Feb-25	13-Feb-25	13-Feb-25	N/A		N/A
Gas Temperature (°C)	18.7	27.3	27.0	39.3	28.1		29.24
% Moisture	0.53	0.73	1.65	1.16	1.02		1.38
Velocity (m/sec)	9.17	8.70	9.20	8.51	8.89		9.64
ACFM	59864	56814	60119	55551	232348		251778
Std. Dry Flow Rate (m ³ /sec)	26.55	24.42	25.63	22.87	99.46	*132	108.58
Tot Part. Dry Basis ref. Cond. (mg/m ³)	5.25	8.30	10.91	10.59	8.68	15.00	6.83
Front Half Particulate (mg/m ³)	3.55	6.47	8.48	7.54	6.51		4.70
Back Half Condensibles (mg/m ³)	1.70	1.83	2.43	3.04	2.25		2.09
Mass Emission Rate (kg/hr)	0.50	0.73	1.00	0.87	3.11	7.67	2.67

* Note: ACFM, m³/sec, and kg/hr, are combined as opposed to averaged.

* Permitted flow rate is 33.0 m³/sec per stack, combined flow rate of 132

* Standard reference conditions are on a dry basis, 20 deg C and pressure at sea level 29.92 inches Hg.

**Average Total Particulate across the four stacks is weighted against individual stack flow

Discussion of Test Results

Test results from the last set of compliance testing was performed in November 2024. Those results are included in the summary tables above for comparison purposes.

Field personnel didn't notice any abnormalities during testing. To the best of our knowledge the plant was operating normally during testing.

Plant production data is included in this report.

All stacks are non-cyclonic and are tested with standard testing methodology.

AVERAGE OF AIR EMISSION TESTS 1 TO 3

Gas Temperature:	66 ° F	19 ° C
Moisture Content (by volume):	0.53 %	
Average Stack Gas Velocity:	30.1 ft/sec	9.2 m/sec
Total Actual Gas Flow Rate:	59864 ACFM	
Dry Gas flow Rate at Reference Conditions:	56251 SCFM	26.5 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	0.002 gr/ft ³	5.25 mg/m ³
Front Half Particulate	0.002 gr/ft ³	3.5 mg/m ³
Back Half Condensibles	0.001 gr/ft ³	1.7 mg/m ³
Mass Emission Rate	1.11 lbs/hr	0.50 kg/hr

SUMMARY OF AIR EMISSION TESTS
TEST 1:

Gas Temperature:	65 ° F	18 ° C
Moisture Content (by volume):	.5 %	
Average Stack Gas Velocity:	30.1 ft/sec	9.2 m/sec
Total Actual Gas Flow Rate:	59905 ACFM	
Dry Gas flow Rate at Reference Conditions:	56413 SCFM	26.6 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.003 gr/ft ³	5.7 mg/m ³
Front Half Particulate	.002 gr/ft ³	4.0 mg/m ³
Back Half Condensibles	.001 gr/ft ³	1.7 mg/m ³
Mass Emission Rate	1.21 lbs/hr	0.55 kg/hr

TEST 2:

Gas Temperature:	65 ° F	18 ° C
Moisture Content (by volume):	.6 %	
Average Stack Gas Velocity:	30.0 ft/sec	9.2 m/sec
Total Actual Gas Flow Rate:	59770 ACFM	
Dry Gas flow Rate at Reference Conditions:	56240 SCFM	26.5 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.002 gr/ft ³	5.3 mg/m ³
Front Half Particulate	.002 gr/ft ³	3.6 mg/m ³
Back Half Condensibles	.001 gr/ft ³	1.7 mg/m ³
Mass Emission Rate	1.12 lbs/hr	0.51 kg/hr

TEST 3:

Gas Temperature:	67 ° F	20 ° C
Moisture Content (by volume):	.6 %	
Average Stack Gas Velocity:	30.1 ft/sec	9.2 m/sec
Total Actual Gas Flow Rate:	59919 ACFM	
Dry Gas flow Rate at Reference Conditions:	56099 SCFM	26.5 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.002 gr/ft ³	4.7 mg/m ³
Front Half Particulate	.001 gr/ft ³	3.0 mg/m ³
Back Half Condensibles	.001 gr/ft ³	1.7 mg/m ³
Mass Emission Rate	0.98 lbs/hr	0.45 kg/hr

DATA FOR TESTS 1 TO 3

Client: Pinnacle Renewable Energy Inc
Plant Location: Smithers BC
Process: Dryer1 Stack 1
Permit Number: RA-6099
Job Number: ME2425-152
Pollution Control Permit: 15.0 mg/m3 49.5 m3/sec
Number of Tests: 3 tests
Minutes per Point: 2.5 minutes

Filter Number:
Date of Test:
Start Time:
Stop Time:
On-line Sampling Time:
Testing Personnel:
Sampler Model:
Barometric Pressure("Hg):
Static Pressure("H₂O):
%CO₂:
%O₂:
%CO:
%N₂:
Diameter of Nozzle(inches):
Meter Factor:
Type-S Pitot Tube Coefficient:
Cross Sectional Area of Stack(ft²):
Impinger Condensate(g):
Weight of Moisture in Silica Gel(g):
Weight of Filter Particulate(g):
Weight of Probe Washings(g):
Weight of Impinger Content Organic(g):
Total Weight of Particulate(g):

TEST 1	TEST 2	TEST 3
P96	P97	P98
13-Feb-25	13-Feb-25	13-Feb-25
10:46	10:47	12:07
11:48	11:49	13:09
60	60	60
DL/CB	DL/CB	DL/CB
980	980	980
28.15	28.15	28.15
-0.20	-0.20	-0.20
0.0	0.0	0.0
21.0	21.0	21.0
0.0	0.0	0.0
79.0	79.0	79.0
0.277	0.277	0.277
0.9997	0.9997	0.9997
0.83365	0.83365	0.83365
33.18	33.18	33.18
3	4	4
1.0	1.0	1.0
0.0005	0.0001	0.0006
0.0042	0.0041	0.0030
0.0020	0.0020	0.0020
0.0067	0.0062	0.0056

Sampling Data for - *TEST 1*
 Pinnacle Renewable Energy Inc
 Dryer1 Stack 1
 Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
A-12	0.27	1.38	33	33	64	2.96	1.06
A-11	0.26	1.43	63	54	56	4.81	0.99
A-10	0.28	1.53	72	55	65	6.61	1.00
A-9	0.27	1.48	74	57	65	8.49	1.03
A-8	0.27	1.48	79	55	62	10.40	1.02
A-7	0.30	1.65	80	58	65	12.30	0.92
A-6	0.30	1.65	74	57	63	14.11	0.94
A-5	0.29	1.60	77	59	64	15.96	0.91
A-4	0.29	1.60	79	63	66	17.72	1.01
A-3	0.28	1.55	81	64	65	19.68	0.90
A-2	0.27	1.50	83	64	65	21.41	0.91
A-1	0.27	1.47	65	64	68	23.12	1.04
B-12	0.24	1.31	73	62	68	25.04	0.92
B-11	0.25	1.37	76	62	67	26.65	0.94
B-10	0.26	1.42	74	62	66	28.34	0.93
B-9	0.27	1.49	78	63	67	30.04	0.99
B-8	0.28	1.55	81	66	69	31.90	0.92
B-7	0.27	1.49	84	65	65	33.65	0.92
B-6	0.29	1.62	84	70	65	35.39	1.00
B-5	0.30	1.69	88	72	64	37.36	0.97
B-4	0.29	1.64	88	73	64	39.32	0.99
B-3	0.28	1.58	89	75	64	41.28	0.92
B-2	0.27	1.53	90	74	64	43.08	0.97
B-1	0.26	1.46	91	74	65	44.94	0.94
						46.71	

Sampling Data for - TEST 2
Pinnacle Renewable Energy Inc
Dryer1 Stack 1
Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
B-12	0.25	1.40	69	73	66	46.84	1.00
B-11	0.26	1.47	74	70	64	48.65	0.98
B-10	0.28	1.58	79	70	65	50.46	0.93
B-9	0.27	1.54	87	72	65	52.24	0.93
B-8	0.27	1.54	84	71	63	54.02	0.95
B-7	0.29	1.66	91	73	65	55.82	0.94
B-6	0.30	1.73	91	79	64	57.69	0.97
B-5	0.30	1.73	93	75	65	59.66	0.97
B-4	0.28	1.62	94	75	64	61.62	0.91
B-3	0.28	1.62	94	76	64	63.40	0.92
B-2	0.27	1.56	97	77	67	65.20	1.04
B-1	0.27	1.57	96	80	64	67.21	1.03
A-12	0.25	1.46	99	81	65	69.20	0.96
A-11	0.25	1.45	97	79	64	70.99	0.93
A-10	0.26	1.52	101	83	65	72.72	0.90
A-9	0.27	1.58	101	82	64	74.45	1.00
A-8	0.26	1.58	102	84	64	76.39	0.98
A-7	0.29	1.70	102	85	64	78.27	0.96
A-6	0.29	1.70	103	85	65	80.22	0.95
A-5	0.30	1.76	103	86	65	82.14	0.97
A-4	0.29	1.71	105	86	65	84.14	1.03
A-3	0.28	1.65	105	87	66	86.23	1.03
A-2	0.27	1.59	104	88	65	88.28	0.96
A-1	0.25	1.47	105	89	64	90.17	0.96
						91.99	

Sampling Data for - *TEST 3*
 Pinnacle Renewable Energy Inc
 Dryer1 Stack 1
 Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
A-12	0.24	1.28	44	45	67	92.34	1.04
A-11	0.26	1.39	46	44	67	94.09	1.02
A-10	0.29	1.54	49	43	68	95.87	1.02
A-9	0.28	1.50	51	44	68	97.75	1.03
A-8	0.27	1.45	52	44	67	99.63	1.03
A-7	0.3	1.61	53	45	67	101.48	0.96
A-6	0.3	1.62	55	45	66	103.29	0.93
A-5	0.29	1.57	56	46	66	105.06	0.99
A-4	0.28	1.51	57	46	67	106.91	0.96
A-3	0.27	1.46	58	47	68	108.68	1.00
A-2	0.26	1.40	59	47	69	110.49	1.05
A-1	0.26	1.41	59	48	68	112.35	1.04
B-12	0.25	1.35	58	49	68	114.20	1.01
B-11	0.26	1.41	59	48	67	115.96	1.05
B-10	0.26	1.41	60	49	67	117.83	0.99
B-9	0.28	1.52	61	50	68	119.60	0.99
B-8	0.29	1.57	62	50	68	121.43	0.95
B-7	0.29	1.58	63	51	69	123.22	0.95
B-6	0.30	1.64	65	52	68	125.01	0.98
B-5	0.29	1.59	67	53	68	126.89	0.96
B-4	0.28	1.54	70	54	67	128.72	0.96
B-3	0.27	1.49	72	55	67	130.51	1.00
B-2	0.26	1.44	73	55	66	132.36	0.96
B-1	0.25	1.39	73	56	66	134.10	1.00
						135.88	



Pinnacle Renewable Energy Inc
Dryer1 Stack 1
Pinnacle Renewable Energy Inc

Data for TEST 1

OVERALL ISOKINETICS - TEST 1 0.965

Delta P:	0.275 "H₂O	Us avg:	30.09 ft/sec
Delta H:	1.520	ACFM:	59905 ft³/min
Tm avg:	529.9 °R	SDCFM:	56413 ft³/min
Ts avg:	524.8 °R	Vm std:	41.16 ft³
Bwo:	0.005	Vm corr:	43.74 ft³
Md:	28.84	Vm:	43.75 ft³
Ms:	28.79	MF:	0.9997
Pb:	28.15 "Hg	PCON:	5.75 mg/m³
Pm:	28.26 "Hg	ERAT:	0.55 kg/hr
Ps:	28.14 "Hg		

Data for TEST 2

OVERALL ISOKINETICS - TEST 2 0.967

Delta P:	0.274 "H₂O	Us avg:	30.02 ft/sec
Delta H:	1.591	ACFM:	59770 ft³/min
Tm avg:	547.1 °R	SDCFM:	56240 ft³/min
Ts avg:	524.7 °R	Vm std:	41.15 ft³
Bwo:	0.006	Vm corr:	45.14 ft³
Md:	28.84	Vm:	45.15 ft³
Ms:	28.78	MF:	0.9997
Pb:	28.15 "Hg	PCON:	5.32 mg/m³
Pm:	28.27 "Hg	ERAT:	0.51 kg/hr
Ps:	28.14 "Hg		

Data for TEST 3

OVERALL ISOKINETICS - TEST 3 0.996

Delta P:	0.274 "H₂O	Us avg:	30.10 ft/sec
Delta H:	1.486	ACFM:	59919 ft³/min
Tm avg:	513.9 °R	SDCFM:	56099 ft³/min
Ts avg:	527.4 °R	Vm std:	42.24 ft³
Bwo:	0.006	Vm corr:	43.53 ft³
Md:	28.84	Vm:	43.54 ft³
Ms:	28.78	MF:	0.9997
Pb:	28.15 "Hg	PCON:	4.68 mg/m³
Pm:	28.26 "Hg	ERAT:	0.45 kg/hr
Ps:	28.14 "Hg		

AVERAGE OF AIR EMISSION TESTS 1 TO 3

Gas Temperature:	81 ° F	27 ° C
Moisture Content (by volume):	0.73 %	
Average Stack Gas Velocity:	28.5 ft/sec	8.7 m/sec
Total Actual Gas Flow Rate:	56814 ACFM	
Dry Gas flow Rate at Reference Conditions:	51747 SCFM	24.4 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	0.004 gr/ft ³	8.3 mg/m ³
Front Half Particulate	0.003 gr/ft ³	6.5 mg/m ³
Back Half Condensibles	0.001 gr/ft ³	1.8 mg/m ³
Mass Emission Rate	1.61 lbs/hr	0.73 kg/hr

SUMMARY OF AIR EMISSION TESTS
TEST 1:

Gas Temperature:	81 ° F	27 ° C
Moisture Content (by volume):	.7 %	
Average Stack Gas Velocity:	28.6 ft/sec	8.7 m/sec
Total Actual Gas Flow Rate:	56949 ACFM	
Dry Gas flow Rate at Reference Conditions:	51852 SCFM	24.5 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.003 gr/ft ³	7.0 mg/m ³
Front Half Particulate	.002 gr/ft ³	5.1 mg/m ³
Back Half Condensibles	.001 gr/ft ³	1.9 mg/m ³
Mass Emission Rate	1.36 lbs/hr	0.62 kg/hr

TEST 2:

Gas Temperature:	83 ° F	28 ° C
Moisture Content (by volume):	.7 %	
Average Stack Gas Velocity:	28.6 ft/sec	8.7 m/sec
Total Actual Gas Flow Rate:	56908 ACFM	
Dry Gas flow Rate at Reference Conditions:	51656 SCFM	24.4 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.003 gr/ft ³	6.6 mg/m ³
Front Half Particulate	.002 gr/ft ³	4.8 mg/m ³
Back Half Condensibles	.001 gr/ft ³	1.8 mg/m ³
Mass Emission Rate	1.28 lbs/hr	0.58 kg/hr

TEST 3:

Gas Temperature:	79 ° F	26 ° C
Moisture Content (by volume):	.7 %	
Average Stack Gas Velocity:	28.4 ft/sec	8.7 m/sec
Total Actual Gas Flow Rate:	56586 ACFM	
Dry Gas flow Rate at Reference Conditions:	51732 SCFM	24.4 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.005 gr/ft ³	11.3 mg/m ³
Front Half Particulate	.004 gr/ft ³	9.5 mg/m ³
Back Half Condensibles	.001 gr/ft ³	1.8 mg/m ³
Mass Emission Rate	2.18 lbs/hr	0.99 kg/hr

DATA FOR TESTS 1 TO 3

Client: Pinnacle Renewable Energy Inc
Plant Location: Smithers BC
Process: Dryer1 Stack 2
Permit Number: RA-6099
Job Number: ME2425-152
Pollution Control Permit: 15.0 mg/m3 49.5 m3/sec
Number of Tests: 3 tests
Minutes per Point: 2.5 minutes

Filter Number:
Date of Test:
Start Time:
Stop Time:
On-line Sampling Time:
Testing Personnel:
Sampler Model:
Barometric Pressure("Hg):
Static Pressure("H₂O):
%CO₂:
%O₂:
%CO:
%N₂:
Diameter of Nozzle(inches):
Meter Factor:
Type-S Pitot Tube Coefficient:
Cross Sectional Area of Stack(ft²):
Impinger Condensate(g):
Weight of Moisture in Silica Gel(g):
Weight of Filter Particulate(g):
Weight of Probe Washings(g):
Weight of Impinger Content Organic(g):
Total Weight of Particulate(g):

TEST 1	TEST 2	TEST 3
P93	P94	P95
13-Feb-25	13-Feb-25	13-Feb-25
10:46	12:21	14:00
11:48	13:23	15:02
60	60	60
CB/CB	CB/CB	CB/CB
1021	1021	1021
28.15	28.15	28.15
-0.19	-0.19	-0.19
0.0	0.0	0.0
21.0	21.0	21.0
0.0	0.0	0.0
79.0	79.0	79.0
0.275	0.275	0.275
0.9972	0.9972	0.9972
0.84182	0.84182	0.84182
33.18	33.18	33.18
5	5	5
1.0	1.0	1.0
0.0002	0.0003	0.0001
0.0053	0.0049	0.0105
0.0020	0.0020	0.0020
0.0075	0.0072	0.0126

Sampling Data for - *TEST 1*
 Pinnacle Renewable Energy Inc
 Dryer1 Stack 2
 Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
A-12	0.28	1.88	61	61	69	39.12	1.01
A-11	0.36	2.38	64	63	81	41.00	0.91
A-10	0.26	1.70	57	51	72	42.90	0.99
A-9	0.28	1.83	60	52	81	44.65	0.98
A-8	0.25	1.63	61	53	81	46.43	0.98
A-7	0.25	1.67	80	55	81	48.11	0.92
A-6	0.24	1.58	66	57	81	49.72	0.99
A-5	0.23	1.52	69	61	82	51.41	0.99
A-4	0.20	1.33	74	58	82	53.07	0.98
A-3	0.20	1.32	69	60	82	54.61	0.97
A-2	0.17	1.12	69	60	82	56.13	0.93
A-1	0.16	1.04	66	64	88	57.47	1.01
B-12	0.27	1.77	67	65	86	58.87	0.91
B-11	0.32	2.11	70	65	85	60.52	0.93
B-10	0.27	1.79	73	65	83	62.36	0.98
B-9	0.28	1.87	73	66	80	64.15	1.04
B-8	0.26	1.74	75	67	82	66.09	0.94
B-7	0.25	1.67	75	67	81	67.79	0.98
B-6	0.23	1.54	76	69	82	69.53	1.00
B-5	0.23	1.54	77	69	81	71.23	1.00
B-4	0.20	1.34	76	70	82	72.94	1.04
B-3	0.21	1.41	77	72	81	74.59	0.97
B-2	0.17	1.14	77	71	83	76.17	1.07
B-1	0.16	1.15	76	71	83	77.74	1.03
						79.20	

Sampling Data for - *TEST 2*
 Pinnacle Renewable Energy Inc
 Dryer1 Stack 2
 Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
B-12	0.29	1.97	70	72	84	79.85	1.01
B-11	0.30	2.04	76	71	83	81.77	0.94
B-10	0.26	1.77	75	71	82	83.60	0.97
B-9	0.27	1.85	77	72	81	85.35	1.04
B-8	0.26	1.78	79	72	83	87.27	0.94
B-7	0.25	1.71	80	73	83	88.97	1.10
B-6	0.23	1.58	82	74	83	90.93	0.91
B-5	0.23	1.58	82	75	83	92.49	1.07
B-4	0.20	1.39	85	86	82	94.33	1.06
B-3	0.20	1.40	85	87	82	96.06	1.00
B-2	0.18	1.25	87	78	82	97.68	0.93
B-1	0.16	1.10	88	81	83	99.10	1.01
A-12	0.28	1.95	89	82	83	100.57	0.94
A-11	0.33	2.30	89	82	83	102.38	1.02
A-10	0.29	2.02	90	81	83	104.50	1.03
A-9	0.28	1.96	94	85	83	106.52	0.97
A-8	0.26	1.82	95	85	83	108.40	1.06
A-7	0.25	1.76	95	87	84	110.37	0.97
A-6	0.22	1.55	96	88	83	112.14	0.99
A-5	0.22	1.56	96	89	83	113.85	0.96
A-4	0.20	1.41	95	89	83	115.50	0.92
A-3	0.22	1.55	97	90	85	117.01	1.08
A-2	0.17	1.20	97	91	84	118.88	0.97
A-1	0.15	1.06	98	92	84	120.35	1.05
						121.85	

Sampling Data for - TEST 3
 Pinnacle Renewable Energy Inc
 Dryer1 Stack 2
 Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
A-12	0.3	1.98	55	54	82	22.14	1.01
A-11	0.29	1.92	57	53	81	24.04	1.01
A-10	0.27	1.79	58	53	80	25.90	1.02
A-9	0.26	1.72	59	52	80	27.72	1.01
A-8	0.26	1.72	60	52	79	29.49	1.01
A-7	0.25	1.66	61	52	79	31.26	1.01
A-6	0.23	1.54	62	53	78	33.01	1.02
A-5	0.23	1.53	62	53	79	34.71	1.09
A-4	0.2	1.33	63	54	80	36.52	1.09
A-3	0.21	1.40	63	54	80	38.21	1.01
A-2	0.18	1.21	64	55	79	39.81	1.04
A-1	0.16	1.07	65	55	78	41.34	1.03
B-12	0.28	1.88	65	56	78	42.78	1.01
B-11	0.33	2.22	66	56	77	44.63	0.97
B-10	0.30	2.02	67	57	78	46.57	1.00
B-9	0.28	1.89	68	57	78	48.48	0.99
B-8	0.26	1.75	69	58	79	50.31	1.00
B-7	0.25	1.69	69	58	79	52.10	1.05
B-6	0.22	1.48	70	59	80	53.93	1.06
B-5	0.22	1.49	71	60	80	55.67	1.06
B-4	0.19	1.28	72	61	81	57.42	0.99
B-3	0.20	1.36	73	62	80	58.94	1.06
B-2	0.16	1.09	73	63	79	60.61	1.01
B-1	0.15	1.02	74	63	78	62.04	1.04
						63.46	



**Pinnacle Renewable Energy Inc
 Dryer1 Stack 2
 Pinnacle Renewable Energy Inc**

Data for TEST 1

OVERALL ISOKINETICS - TEST 1 0.981

Delta P:	0.236 "H₂O	Us avg:	28.61 ft/sec
Delta H:	1.586	ACFM:	56949 ft³/min
Tm avg:	526.7 °R	SDCFM:	51852 ft³/min
Ts avg:	541.3 °R	Vm std:	37.85 ft³
Bwo:	0.007	Vm corr:	39.97 ft³
Md:	28.84	Vm:	40.08 ft³
Ms:	28.76	MF:	0.9972
Pb:	28.15 "Hg	PCON:	7.00 mg/m³
Pm:	28.27 "Hg	ERAT:	0.62 kg/hr
Ps:	28.14 "Hg		

Data for TEST 2

OVERALL ISOKINETICS - TEST 2 0.997

Delta P:	0.235 "H₂O	Us avg:	28.59 ft/sec
Delta H:	1.648	ACFM:	56908 ft³/min
Tm avg:	544.4 °R	SDCFM:	51656 ft³/min
Ts avg:	543.0 °R	Vm std:	38.38 ft³
Bwo:	0.007	Vm corr:	41.88 ft³
Md:	28.84	Vm:	42.00 ft³
Ms:	28.76	MF:	0.9972
Pb:	28.15 "Hg	PCON:	6.62 mg/m³
Pm:	28.27 "Hg	ERAT:	0.58 kg/hr
Ps:	28.14 "Hg		

Data for TEST 3

OVERALL ISOKINETICS - TEST 3 1.025

Delta P:	0.234 "H₂O	Us avg:	28.42 ft/sec
Delta H:	1.585	ACFM:	56586 ft³/min
Tm avg:	520.8 °R	SDCFM:	51732 ft³/min
Ts avg:	539.3 °R	Vm std:	39.47 ft³
Bwo:	0.007	Vm corr:	41.20 ft³
Md:	28.84	Vm:	41.32 ft³
Ms:	28.76	MF:	0.9972
Pb:	28.15 "Hg	PCON:	11.27 mg/m³
Pm:	28.27 "Hg	ERAT:	0.99 kg/hr
Ps:	28.14 "Hg		

AVERAGE OF AIR EMISSION TESTS 1 TO 3

Gas Temperature:	81 ° F	27 ° C
Moisture Content (by volume):	1.65 %	
Average Stack Gas Velocity:	30.2 ft/sec	9.2 m/sec
Total Actual Gas Flow Rate:	60119 ACFM	
Dry Gas flow Rate at Reference Conditions:	54304 SCFM	25.6 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	0.005 gr/ft ³	10.9 mg/m ³
Front Half Particulate	0.004 gr/ft ³	8.5 mg/m ³
Back Half Condensibles	0.001 gr/ft ³	2.4 mg/m ³
Mass Emission Rate	2.21 lbs/hr	1.00 kg/hr

SUMMARY OF AIR EMISSION TESTS
TEST 1:

Gas Temperature:	80 ° F	27 ° C
Moisture Content (by volume):	1.9 %	
Average Stack Gas Velocity:	29.8 ft/sec	9.1 m/sec
Total Actual Gas Flow Rate:	59342 ACFM	
Dry Gas flow Rate at Reference Conditions:	53482 SCFM	25.2 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.006 gr/ft ³	13.1 mg/m ³
Front Half Particulate	.005 gr/ft ³	10.3 mg/m ³
Back Half Condensibles	.001 gr/ft ³	2.8 mg/m ³
Mass Emission Rate	2.63 lbs/hr	1.19 kg/hr

TEST 2:

Gas Temperature:	84 ° F	29 ° C
Moisture Content (by volume):	1.3 %	
Average Stack Gas Velocity:	30.5 ft/sec	9.3 m/sec
Total Actual Gas Flow Rate:	60627 ACFM	
Dry Gas flow Rate at Reference Conditions:	54638 SCFM	25.8 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.004 gr/ft ³	10.2 mg/m ³
Front Half Particulate	.003 gr/ft ³	7.5 mg/m ³
Back Half Condensibles	.001 gr/ft ³	2.7 mg/m ³
Mass Emission Rate	2.09 lbs/hr	0.95 kg/hr

TEST 3:

Gas Temperature:	78 ° F	25 ° C
Moisture Content (by volume):	1.7 %	
Average Stack Gas Velocity:	30.3 ft/sec	9.2 m/sec
Total Actual Gas Flow Rate:	60388 ACFM	
Dry Gas flow Rate at Reference Conditions:	54791 SCFM	25.9 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.004 gr/ft ³	9.4 mg/m ³
Front Half Particulate	.003 gr/ft ³	7.6 mg/m ³
Back Half Condensibles	.001 gr/ft ³	1.8 mg/m ³
Mass Emission Rate	1.93 lbs/hr	0.88 kg/hr

DATA FOR TESTS 1 TO 3

Client: Pinnacle Renewable Energy Inc
Plant Location: Smithers BC
Process: Dryer1 Stack 3
Permit Number: RA-6099
Job Number: ME2425-152
Pollution Control Permit: 15.0 mg/m3 49.5 m3/sec
Number of Tests: 3 tests
Minutes per Point: 2.5 minutes

Filter Number:
Date of Test:
Start Time:
Stop Time:
On-line Sampling Time:
Testing Personnel:
Sampler Model:
Barometric Pressure("Hg):
Static Pressure("H₂O):
%CO₂:
%O₂:
%CO:
%N₂:
Diameter of Nozzle(inches):
Meter Factor:
Type-S Pitot Tube Coefficient:
Cross Sectional Area of Stack(ft²):
Impinger Condensate(g):
Weight of Moisture in Silica Gel(g):
Weight of Filter Particulate(g):
Weight of Probe Washings(g):
Weight of Impinger Content Organic(g):
Total Weight of Particulate(g):

TEST 1	TEST 2	TEST 3
Q2	Q3	Q4
13-Feb-25	13-Feb-25	13-Feb-25
11:10	12:45	14:20
12:12	13:48	15:23
60	60	60
DL/DB	DL/DB	DL/DB
955	955	955
28.15	28.15	28.15
-0.23	-0.23	-0.23
0.0	0.0	0.0
21.0	21.0	21.0
0.0	0.0	0.0
79.0	79.0	79.0
0.270	0.270	0.270
0.9973	0.9973	0.9973
0.83867	0.83867	0.83867
33.18	33.18	33.18
14	10	13
1.6	1.4	1.5
0.0018	0.0014	0.0010
0.0092	0.0070	0.0075
0.0030	0.0030	0.0020
0.0140	0.0114	0.0105

Sampling Data for - TEST 1
Pinnacle Renewable Energy Inc
Dryer1 Stack 3
Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
A-12	0.23	1.31	21	21	68	55.93	0.92
A-11	0.23	1.30	38	23	80	57.30	0.90
A-10	0.24	1.37	41	25	81	58.65	0.95
A-9	0.25	1.42	40	26	81	60.10	0.94
A-8	0.23	1.31	42	29	82	61.57	0.95
A-7	0.24	1.38	44	33	81	63.00	0.97
A-6	0.25	1.45	48	34	81	64.50	0.94
A-5	0.27	1.56	53	35	80	66.00	1.02
A-4	0.29	1.70	58	39	80	67.70	1.04
A-3	0.30	1.77	62	40	80	69.50	0.98
A-2	0.30	1.78	67	46	83	71.24	1.00
A-1	0.27	1.62	72	49	82	73.03	0.98
B-12	0.24	1.45	75	51	79	74.70	1.01
B-11	0.24	1.45	81	54	80	76.35	1.02
B-10	0.25	1.51	82	56	82	78.02	0.95
B-9	0.24	1.47	84	58	82	79.61	1.00
B-8	0.23	1.41	88	62	80	81.25	0.98
B-7	0.24	1.48	90	63	81	82.85	0.99
B-6	0.24	1.49	92	66	81	84.50	1.02
B-5	0.26	1.62	93	67	80	86.20	0.94
B-4	0.27	1.68	94	69	81	87.85	0.98
B-3	0.29	1.82	96	71	81	89.60	0.99
B-2	0.30	1.88	96	73	81	91.43	1.01
B-1	0.30	1.88	97	74	81	93.33	1.00
						95.23	

Sampling Data for - TEST 2
Pinnacle Renewable Energy Inc
Dryer1 Stack 3
Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
B-12	0.24	1.47	71	71	82	95.90	1.00
B-11	0.24	1.48	79	70	81	97.56	1.01
B-10	0.25	1.54	80	70	82	99.25	0.94
B-9	0.26	1.62	87	72	82	100.85	1.06
B-8	0.26	1.63	88	75	80	102.70	1.02
B-7	0.27	1.69	91	77	83	104.50	0.98
B-6	0.26	1.63	93	78	81	106.26	1.06
B-5	0.28	1.75	94	79	82	108.13	0.96
B-4	0.29	1.83	95	81	82	109.90	1.01
B-3	0.30	1.90	96	83	82	111.80	0.97
B-2	0.28	1.77	97	85	83	113.65	0.94
B-1	0.29	1.85	101	84	81	115.40	1.06
A-12	0.25	1.59	103	85	84	117.40	0.99
A-11	0.25	1.59	104	86	84	119.14	1.02
A-10	0.27	1.72	108	88	83	120.94	0.98
A-9	0.25	1.61	110	91	84	122.75	1.04
A-8	0.25	1.61	111	93	85	124.60	1.07
A-7	0.26	1.68	112	96	86	126.50	0.95
A-6	0.26	1.68	110	95	85	128.23	1.01
A-5	0.28	1.80	110	96	86	130.07	0.97
A-4	0.29	1.86	111	95	89	131.90	1.05
A-3	0.30	1.92	112	96	86	133.92	1.01
A-2	0.28	1.79	112	95	85	135.90	1.01
A-1	0.28	1.79	112	95	86	137.81	1.00
						139.70	

Sampling Data for - TEST 3
 Pinnacle Renewable Energy Inc
 Dryer1 Stack 3
 Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
A-12	0.24	1.42	55	56	83	41.70	1.08
A-11	0.24	1.45	60	59	78	43.43	0.94
A-10	0.25	1.51	62	60	78	44.95	1.05
A-9	0.26	1.57	63	61	80	46.70	0.98
A-8	0.26	1.57	68	62	79	48.36	0.96
A-7	0.27	1.65	75	62	80	50.00	0.95
A-6	0.27	1.67	82	64	79	51.66	0.99
A-5	0.27	1.67	85	66	79	53.40	0.98
A-4	0.28	1.75	90	68	77	55.14	0.97
A-3	0.29	1.83	93	69	75	56.90	1.01
A-2	0.3	1.89	93	70	77	58.78	1.04
A-1	0.3	1.90	96	73	78	60.75	0.97
B-12	0.23	1.45	99	75	78	62.60	1.02
B-11	0.23	1.45	101	78	78	64.30	0.98
B-10	0.25	1.58	101	78	78	65.95	1.00
B-9	0.26	1.67	103	82	78	67.70	1.00
B-8	0.26	1.67	105	83	77	69.50	1.00
B-7	0.27	1.73	105	84	78	71.30	0.98
B-6	0.28	1.81	106	86	77	73.10	1.03
B-5	0.28	1.81	109	87	76	75.03	1.01
B-4	0.30	1.94	109	88	78	76.94	1.01
B-3	0.29	1.88	110	89	77	78.90	1.00
B-2	0.29	1.88	108	86	76	80.82	1.04
B-1	0.28	1.82	108	86	75	82.80	1.01
						84.70	



Pinnacle Renewable Energy Inc
 Dryer1 Stack 3
 Pinnacle Renewable Energy Inc

Data for **TEST 1**

OVERALL ISOKINETICS - TEST 1 0.978

Delta P:	0.258 "H ₂ O	Us avg:	29.81 ft/sec
Delta H:	1.546	ACFM:	59342 ft ³ /min
Tm avg:	518.7 °R	SDCFM:	53482 ft ³ /min
Ts avg:	540.3 °R	Vm std:	37.69 ft ³
Bwo:	0.019	Vm corr:	39.19 ft ³
Md:	28.84	Vm:	39.30 ft ³
Ms:	28.63	MF:	0.9973
Pb:	28.15 "Hg	PCON:	13.12 mg/m ³
Pm:	28.26 "Hg	ERAT:	1.19 kg/hr
Ps:	28.13 "Hg		

Data for **TEST 2**

OVERALL ISOKINETICS - TEST 2 1.005

Delta P:	0.268 "H ₂ O	Us avg:	30.45 ft/sec
Delta H:	1.700	ACFM:	60627 ft ³ /min
Tm avg:	552.1 °R	SDCFM:	54638 ft ³ /min
Ts avg:	543.5 °R	Vm std:	39.48 ft ³
Bwo:	0.013	Vm corr:	43.68 ft ³
Md:	28.84	Vm:	43.80 ft ³
Ms:	28.69	MF:	0.9973
Pb:	28.15 "Hg	PCON:	10.20 mg/m ³
Pm:	28.28 "Hg	ERAT:	0.95 kg/hr
Ps:	28.13 "Hg		

Data for **TEST 3**

OVERALL ISOKINETICS - TEST 3 1.001

Delta P:	0.268 "H ₂ O	Us avg:	30.33 ft/sec
Delta H:	1.690	ACFM:	60388 ft ³ /min
Tm avg:	542.5 °R	SDCFM:	54791 ft ³ /min
Ts avg:	537.9 °R	Vm std:	39.45 ft ³
Bwo:	0.017	Vm corr:	42.88 ft ³
Md:	28.84	Vm:	43.00 ft ³
Ms:	28.66	MF:	0.9973
Pb:	28.15 "Hg	PCON:	9.40 mg/m ³
Pm:	28.27 "Hg	ERAT:	0.88 kg/hr
Ps:	28.13 "Hg		

Pinnacle Renewable Energy Inc.
Dryer1 Stack 4
Smithers BC

13-Feb-25

Permit Number: RA-6099

AVERAGE OF AIR EMISSION TESTS 1 TO 3

Gas Temperature:	103 ° F	39 ° C
Moisture Content (by volume):	1.16 %	
Average Stack Gas Velocity:	27.9 ft/sec	8.5 m/sec
Total Actual Gas Flow Rate:	55551 ACFM	
Dry Gas flow Rate at Reference Conditions:	48451 SCFM	22.9 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	0.005 gr/ft ³	10.6 mg/m ³
Front Half Particulate	0.003 gr/ft ³	7.6 mg/m ³
Back Half Condensibles	0.001 gr/ft ³	3.0 mg/m ³
Mass Emission Rate	1.92 lbs/hr	0.87 kg/hr

SUMMARY OF AIR EMISSION TESTS

TEST 1:

Gas Temperature:	97 ° F	36 ° C
Moisture Content (by volume):	1.1 %	
Average Stack Gas Velocity:	27.6 ft/sec	8.4 m/sec
Total Actual Gas Flow Rate:	54988 ACFM	
Dry Gas flow Rate at Reference Conditions:	48514 SCFM	22.9 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.003 gr/ft ³	6.4 mg/m ³
Front Half Particulate	.002 gr/ft ³	4.4 mg/m ³
Back Half Condensibles	.001 gr/ft ³	2.0 mg/m ³
Mass Emission Rate	1.17 lbs/hr	0.53 kg/hr

TEST 2:

Gas Temperature:	103 ° F	40 ° C
Moisture Content (by volume):	1.2 %	
Average Stack Gas Velocity:	27.9 ft/sec	8.5 m/sec
Total Actual Gas Flow Rate:	55465 ACFM	
Dry Gas flow Rate at Reference Conditions:	48317 SCFM	22.8 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.005 gr/ft ³	11.7 mg/m ³
Front Half Particulate	.004 gr/ft ³	8.7 mg/m ³
Back Half Condensibles	.001 gr/ft ³	3.1 mg/m ³
Mass Emission Rate	2.12 lbs/hr	0.96 kg/hr

TEST 3:

Gas Temperature:	108 ° F	42 ° C
Moisture Content (by volume):	1.2 %	
Average Stack Gas Velocity:	28.2 ft/sec	8.6 m/sec
Total Actual Gas Flow Rate:	56199 ACFM	
Dry Gas flow Rate at Reference Conditions:	48522 SCFM	22.9 m ³ /sec
Total Particulate Concentration:		
Dry Basis Actual at Reference Conditions	.006 gr/ft ³	13.6 mg/m ³
Front Half Particulate	.004 gr/ft ³	9.6 mg/m ³
Back Half Condensibles	.002 gr/ft ³	4.0 mg/m ³
Mass Emission Rate	2.48 lbs/hr	1.12 kg/hr

DATA FOR TESTS 1 TO 3

Client: Pinnacle Renewable Energy Inc.
Plant Location: Smithers BC
Process: Dryer1 Stack 4
Permit Number: RA-6099
Job Number: ME2425-152
Pollution Control Permit: 15.0 mg/m3 49.5 m3/sec
Number of Tests: 3 tests
Minutes per Point: 2.5 minutes

Filter Number:
Date of Test:
Start Time:
Stop Time:
On-line Sampling Time:
Testing Personnel:
Sampler Model:
Barometric Pressure("Hg):
Static Pressure("H₂O):
%CO₂:
%O₂:
%CO:
%N₂:
Diameter of Nozzle(inches):
Meter Factor:
Type-S Pitot Tube Coefficient:
Cross Sectional Area of Stack(ft²):
Impinger Condensate(g):
Weight of Moisture in Silica Gel(g):
Weight of Filter Particulate(g):
Weight of Probe Washings(g):
Weight of Impinger Content Organic(g):
Total Weight of Particulate(g):

TEST 1	TEST 2	TEST 3
Q5	Q6	Q7
13-Feb-25	13-Feb-25	13-Feb-25
11:11	12:45	14:20
12:13	13:47	15:22
60	60	60
DB/DL	DB/DL	DB/DL
1039	1039	955
28.15	28.15	28.15
-0.16	-0.16	-0.16
0.0	0.0	0.0
21.0	21.0	21.0
0.0	0.0	0.0
79.0	79.0	79.0
0.270	0.270	0.270
1.0043	1.0043	0.9994
0.83829	0.83829	0.83829
33.18	33.18	33.18
7	8	8
1.0	1.0	1.0
0.0001	0.0002	0.0003
0.0042	0.0083	0.0092
0.0020	0.0030	0.0040
0.0063	0.0115	0.0135

Sampling Data for - TEST 1
Pinnacle Renewable Energy Inc.
Dryer1 Stack 4
Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
A-12	0.26	1.00	40	40	96	30.01	0.95
A-11	0.28	1.11	48	40	93	31.52	1.00
A-10	0.24	0.96	52	40	93	33.20	1.03
A-9	0.18	0.72	58	42	93	34.81	0.96
A-8	0.16	0.65	64	43	92	36.11	0.97
A-7	0.16	0.65	69	45	93	37.36	0.99
A-6	0.16	0.66	73	46	92	38.64	0.98
A-5	0.17	0.70	79	50	93	39.92	1.02
A-4	0.24	1.00	83	52	95	41.30	1.05
A-3	0.26	1.10	87	54	96	43.00	1.01
A-2	0.26	1.10	90	59	97	44.71	1.00
A-1	0.25	1.05	91	63	98	46.42	0.99
B-12	0.25	1.05	92	67	99	48.08	0.97
B-11	0.27	1.14	93	68	100	49.72	0.98
B-10	0.25	1.06	94	69	100	51.43	0.98
B-9	0.19	0.81	96	71	99	53.09	0.98
B-8	0.17	0.72	97	72	99	54.54	0.97
B-7	0.16	0.68	98	73	99	55.90	0.99
B-6	0.16	0.68	99	74	99	57.25	1.02
B-5	0.18	0.77	100	75	99	58.64	1.00
B-4	0.22	0.94	101	76	99	60.09	0.96
B-3	0.26	1.12	101	78	99	61.63	0.97
B-2	0.25	1.07	102	80	99	63.32	1.02
B-1	0.25	1.07	103	80	100	65.07	0.97
						66.73	

Sampling Data for - TEST 2
Pinnacle Renewable Energy Inc.
Dryer1 Stack 4
Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
B-12	0.27	1.15	84	84	98	66.96	1.00
B-11	0.28	1.20	89	86	99	68.72	0.97
B-10	0.24	1.03	94	87	99	70.48	1.00
B-9	0.22	0.95	104	88	101	72.17	0.99
B-8	0.17	0.74	105	89	102	73.78	0.97
B-7	0.17	0.74	106	90	102	75.16	1.02
B-6	0.16	0.70	107	91	101	76.62	1.00
B-5	0.17	0.74	108	92	101	78.01	0.99
B-4	0.22	0.96	109	93	101	79.43	1.00
B-3	0.25	1.09	111	94	102	81.07	1.00
B-2	0.25	1.09	112	95	102	82.82	0.99
B-1	0.26	1.14	113	96	103	84.55	1.02
A-12	0.27	1.18	113	96	102	86.38	1.00
A-11	0.27	1.18	114	97	103	88.20	1.00
A-10	0.25	1.10	114	98	104	90.02	0.97
A-9	0.23	1.01	115	99	104	91.73	0.99
A-8	0.19	0.83	116	100	105	93.40	0.99
A-7	0.18	0.79	117	101	106	94.92	1.00
A-6	0.18	0.79	118	102	106	96.41	0.99
A-5	0.17	0.75	118	102	106	97.89	0.99
A-4	0.16	0.70	119	103	107	99.33	0.99
A-3	0.20	0.88	119	103	107	100.73	1.06
A-2	0.24	1.06	120	103	107	102.41	1.01
A-1	0.25	1.10	120	104	107	104.16	0.99
						105.91	

Sampling Data for - TEST 3
 Pinnacle Renewable Energy Inc.
 Dryer1 Stack 4
 Smithers BC

13-Feb-25

SAMPLE POINT	VELOCITY HEAD ("H ₂ O)	ORIFICE PRESSURE ("H ₂ O)	DRY GAS METER		STACK GAS TEMP (° F)	GAS SAMPLE VOLUME (ft ³)	ISOKINETICS
			TEMP IN (° F)	TEMP OUT (° F)			
A-12	0.26	1.07	77	81	110	6.04	0.98
A-11	0.28	1.17	85	84	109	7.71	1.00
A-10	0.25	1.05	89	85	109	9.50	1.00
A-9	0.22	0.93	90	86	109	11.20	0.99
A-8	0.18	0.76	93	87	109	12.78	0.99
A-7	0.17	0.72	94	88	109	14.22	1.01
A-6	0.17	0.72	95	89	109	15.65	1.00
A-5	0.16	0.68	96	90	110	17.06	0.98
A-4	0.23	0.98	98	91	110	18.41	0.99
A-3	0.25	1.07	101	92	110	20.04	0.99
A-2	0.26	1.11	102	92	109	21.75	0.99
A-1	0.26	1.11	103	93	109	23.50	0.98
B-12	0.25	1.07	104	94	109	25.24	1.01
B-11	0.27	1.16	107	95	109	27.00	0.99
B-10	0.26	1.12	110	96	110	28.79	0.99
B-9	0.23	0.99	111	97	110	30.55	1.10
B-8	0.21	0.91	112	98	108	34.03	1.10
B-7	0.19	0.83	113	99	107	35.80	0.99
B-6	0.16	0.70	114	100	106	37.32	1.01
B-5	0.16	0.70	114	101	105	38.75	1.00
B-4	0.18	0.79	115	102	105	40.17	0.95
B-3	0.23	1.01	116	103	104	41.60	0.98
B-2	0.25	1.10	117	104	106	43.27	0.97
B-1	0.26	1.14	118	106	107	45.00	0.98
						46.77	



Pinnacle Renewable Energy Inc.
Dryer1 Stack 4
Pinnacle Renewable Energy Inc.

Data for TEST 1

OVERALL ISOKINETICS - TEST 1 0.989

Delta P:	0.216 "H₂O	Us avg:	27.62 ft/sec
Delta H:	0.909	ACFM:	54988 ft³/min
Tm avg:	532.2 °R	SDCFM:	48514 ft³/min
Ts avg:	556.8 °R	Vm std:	34.50 ft³
Bwo:	0.011	Vm corr:	36.88 ft³
Md:	28.84	Vm:	36.72 ft³
Ms:	28.72	MF:	1.0043
Pb:	28.15 "Hg	PCON:	6.45 mg/m³
Pm:	28.22 "Hg	ERAT:	0.53 kg/hr
Ps:	28.14 "Hg		

Data for TEST 2

OVERALL ISOKINETICS - TEST 2 0.997

Delta P:	0.217 "H₂O	Us avg:	27.86 ft/sec
Delta H:	0.954	ACFM:	55465 ft³/min
Tm avg:	562.9 °R	SDCFM:	48317 ft³/min
Ts avg:	563.1 °R	Vm std:	34.61 ft³
Bwo:	0.012	Vm corr:	39.12 ft³
Md:	28.84	Vm:	38.95 ft³
Ms:	28.71	MF:	1.0043
Pb:	28.15 "Hg	PCON:	11.73 mg/m³
Pm:	28.22 "Hg	ERAT:	0.96 kg/hr
Ps:	28.14 "Hg		

Data for TEST 3

OVERALL ISOKINETICS - TEST 3 0.999

Delta P:	0.221 "H₂O	Us avg:	28.23 ft/sec
Delta H:	0.954	ACFM:	56199 ft³/min
Tm avg:	579.3 °R	SDCFM:	48522 ft³/min
Ts avg:	568.3 °R	Vm std:	34.99 ft³
Bwo:	0.012	Vm corr:	40.71 ft³
Md:	28.84	Vm:	40.73 ft³
Ms:	28.71	MF:	0.9994
Pb:	28.15 "Hg	PCON:	13.62 mg/m³
Pm:	28.22 "Hg	ERAT:	1.12 kg/hr
Ps:	28.14 "Hg		

Air Emission Monitoring Procedure **State Of Oregon Method 7**

Particulate Sampling (Napp-Baldwin Model 31 Sampler)

Particulate sampling and gas velocity measurements were conducted using a Napp-Baldwin Model 31 stack sampler in accordance with the methods specified in State of Oregon Method 7 (See Figure 1). The State of Oregon Method 7 sampling train is a modified Method 5 sample train with the addition of a non heated filter in-between the third and fourth impinger.

The air discharge was sampled isokinetically at the centroid of a series of equal area segments across the duct or stack. The stack gas velocity and temperature were recorded during the sample collection period with a calibrated pitot tube and thermocouple mounted on the sampling probe. The sample was delivered from the probe to a cyclone and a filter holder containing a 110mm Type A glass fiber filter. The gas sample was then drawn in through a series of four glass impingers which condensed and absorbed the water from the gas. A leakless vacuum pump carried the sampled gas through a dry gas test meter where the volume, temperature, and pressure were measured; and finally through a flow indicating orifice which allowed for the rapid adjustment to isokinetic sampling rates.

At the end of each test, the probe interior, cyclone and connecting tubing from the probe to the filter housing were rinsed with distilled water and acetone. These washings were evaporated to dryness and the resulting solids were weighed. The weight of the cyclone flask and the filter was used together with the weight of solids in the washings to calculate the filterable particulate concentration. The moisture content of the stack gas was determined from the quantity of water condensed in the impingers and absorbed in the silica gel.

Condensable Organics are collected in the impinger train and a rinsing procedure is employed utilizing solvents such as Hexane or Methylene Chloride in between tests. The rinsings and condensate are forwarded to a laboratory accredited to perform the analysis in accordance with the method and a copy of that report is included in the Appendix of any report issued.

O₂, CO₂, CO (where applicable)

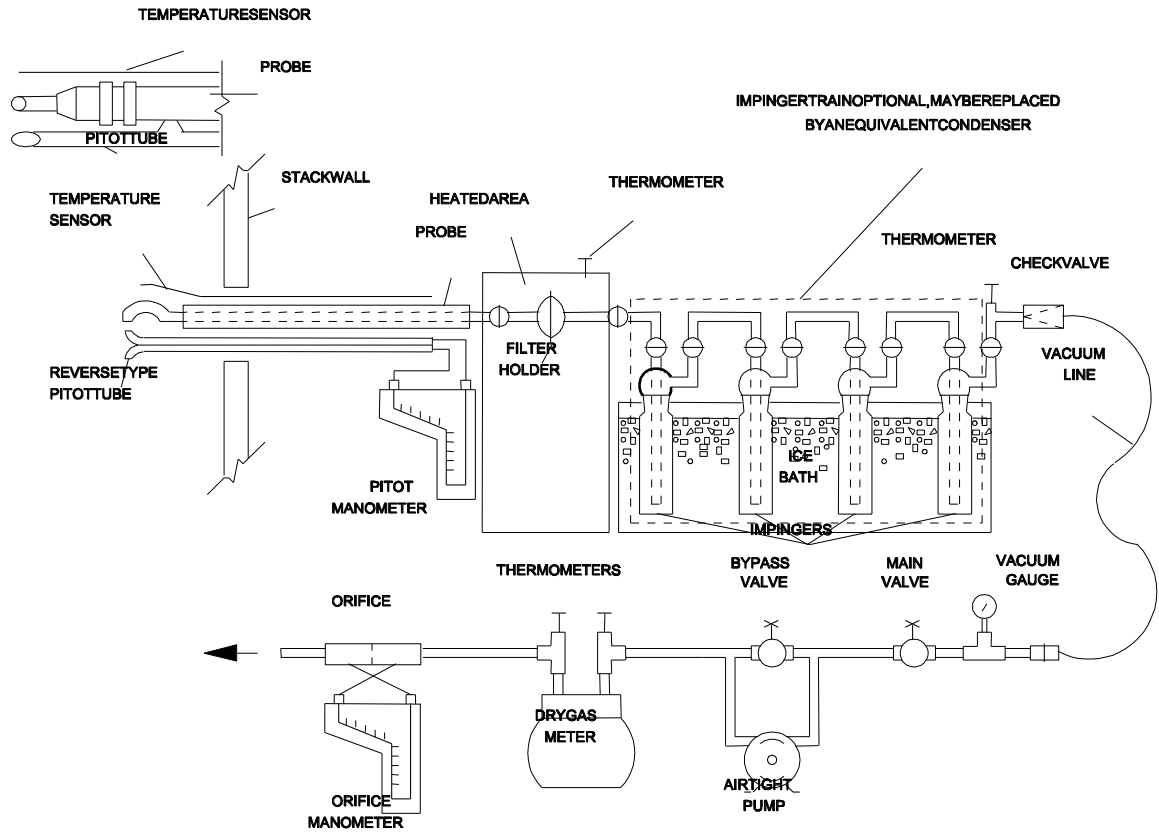
O₂, CO₂, and CO were found using either Fuji Analytical Analyzer by means of infrared and paramagnetic technology (EPA 3A) or by fyrite (EPA Method 3).

NO_x (where applicable)

NO_x was found using and API Model 252 NO_x analyzer that utilizes chemiluminescent technology. Stack gas was Samples were taken over a minimum period of three hours.

VOC's (where applicable)

Hydrocarbons were measured in accordance with EPA method 25A. Samples were drawn in one hour test runs using a total hydrocarbon analyzer that utilizes Flame Ionization Technology.



Modified EPA Method 5 Diagram (State of Oregon Method 7)- Figure 1

GENERAL CALCULATIONS

Carry out calculations, retaining at least one extra decimal figure beyond that of the acquired data. Round off figures after the final calculation. Other forms of the equations may be used as long as they give equivalent results.

Nomenclature.

- A_n = Cross-sectional area of nozzle, m^2 (ft^2).
 B_{ws} = Water vapor in the gas stream, proportion by volume.
 C_a = Acetone blank residue concentration, mg/g .
 c_s = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, $g/dscm$ ($g/dscf$).
 I = Percent of isokinetic sampling.
 L_a = Maximum acceptable leakage rate for either a pretest leak check or for a leak check following a component change; equal to $0.00057 m^3/min$ ($0.02 cfm$) or 4 percent of the average sampling rate, whichever is less.
 L_i = Individual leakage rate observed during the leak check conducted prior to the " i^{th} " component change ($i = 1, 2, 3...n$), m^3/min (cfm).
 L_p = Leakage rate observed during the post-test leak check, m^3/min (cfm).
 m_a = Mass of residue of acetone after evaporation, mg .
 m_n = Total amount of particulate matter collected, mg .
 M_w = Molecular weight of water, $18.0 g/g\text{-mole}$ ($18.0 lb/lb\text{-mole}$).
 P_{bar} = Barometric pressure at the sampling site, $mm Hg$ ($in. Hg$).
 P_s = Absolute stack gas pressure, $mm Hg$ ($in. Hg$).
 P_{std} = Standard absolute pressure, $760 mm Hg$ ($29.92 in. Hg$).
 R = Ideal gas constant, $0.06236 \frac{[(mmHg)(m^3)]}{[(^{\circ}K)(g\text{-mole})]}$
 $\{21.85 \frac{[(in. Hg)(ft^3)]}{[(^{\circ}R)(lb\text{-mole})]}\}$.
 T_m = Absolute average DGM temperature (see Figure 5-2), $^{\circ}K$ ($^{\circ}R$).
 T_s = Absolute average stack gas temperature (see Figure 5-2), $^{\circ}K$ ($^{\circ}R$).
 T_{std} = Standard absolute temperature, $293^{\circ}K$ ($528^{\circ}R$).
 V_a = Volume of acetone blank, ml .
 V_{aw} = Volume of acetone used in wash, ml .
 V_{lc} = Total volume liquid collected in impingers and silica gel (see Figure 5-3), ml .
 V_m = Volume of gas sample as measured by dry gas meter, dcm (dcf).
 $V_{m(std)}$ = Volume of gas sample measured by the dry gas meter, corrected to standard conditions, $dscm$ ($dscf$).
 $V_{w(std)}$ = Volume of water vapor in the gas sample, corrected to standard conditions, scm (scf).
 v_s = Stack gas velocity, calculated by Method 2, Equation 2-9, using data obtained from Method 5, m/sec (ft/sec).
 W_a = Weight of residue in acetone wash, mg .
 Y = Dry gas meter calibration factor.
 ΔH = Average pressure differential across the orifice meter (see Figure 5-2), $mm H_2O$ ($in. H_2O$).
 ρ_a = Density of acetone, mg/ml (see label on bottle).
 ρ_w = Density of water, $0.9982 g/ml$ ($0.002201 lb/ml$).
 θ = Total sampling time, min .
 θ_1 = Sampling time interval, from the beginning of a run until the first component change, min .
 θ_i = Sampling time interval, between two successive component changes, beginning with the interval between the first and second changes, min .
 θ_p = Sampling time interval, from the final (n^{th}) component change until the end of the sampling run, min .
 13.6 = Specific gravity of mercury.
 60 = Sec/min .
 100 = Conversion to percent.

Average Dry Gas Meter Temperature and Average Orifice Pressure Drop.

Dry Gas Volume. Correct the sample volume measured by the dry gas meter to standard conditions (20°C, 760 mm Hg or 68°F, 29.92 in. Hg) by using Equation 5-1.

$$V_{m(\text{std})} = V_m Y \left(\frac{T_{\text{std}}}{T_m} \right) \left[\frac{P_{\text{bar}} + \frac{\Delta H}{13.6}}{P_{\text{std}}} \right] \quad \text{Eq. 5-1}$$

$$= K_1 V_m Y \frac{P_{\text{bar}} + \left(\frac{\Delta H}{13.6} \right)}{T_m}$$

where:

$$K_1 = 0.3858 \text{ }^\circ\text{K/mm Hg for metric units,}$$

$$= 17.64 \text{ }^\circ\text{R/in. Hg for English units.}$$

NOTE: Equation 5-1 can be used as written unless leakage rate observed during any of the mandatory leak checks (i.e., the post-test leak check or leak checks conducted prior to component changes) exceeds L_a . If L_p or L_i exceeds L_a , Equation 5-1 must be modified as follows:

(a) Case I. No component changes made during sampling run. In this case, replace V_m in Equation 5-1 with the expression:

$$[V_m - (L_p - L_a) \theta]$$

(b) Case II. One or more component changes made during the sampling run. In this case, replace V_m in Equation 5-1 by the expression:

$$\left[V_m - (L_1 - L_a) \theta_1 - \sum_{i=2}^n (L_i - L_a) \theta_i - (L_p - L_a) \theta_p \right]$$

and substitute only for those leakage rates (L_i or L_p) which exceed L_a .

Volume of Water Vapor.

$$V_{w(\text{std})} = \frac{V_{lc} \rho_w R T_{\text{std}}}{M_w P_{\text{std}}} = K_2 V_{lc} \quad \text{Eq. 5-2}$$

where:

$$K_2 = 0.001333 \text{ m}^3/\text{ml for metric units,}$$

$$= 0.04707 \text{ ft}^3/\text{ml for English units.}$$

Moisture Content.

$$B_{ws} = \frac{V_{w(std)}}{V_{m(std)} + V_{w(std)}} \quad \text{Eq. 5-3}$$

Acetone Blank Concentration.

$$C_a = \frac{m_a}{V_a \rho_a} \quad \text{Eq. 5-4}$$

Acetone Wash Blank.

$$W_a = C_a V_{aw} \rho_a \quad \text{Eq. 5-5}$$

Total Particulate Weight. Determine the total particulate matter catch from the sum of the weights obtained from Containers 1 and 2 less the acetone blank (see Figure 5-3).

Particulate Concentration.

$$C_s = (0.001 \text{ g/mg})(m_n / V_{m(std)}) \quad \text{Eq. 5-6}$$

Conversion Factors:

<u>From</u>	<u>To</u>	<u>Multiply by</u>
scf	m ³	0.02832
g/ft ³	gr/ft ³	15.43
g/ft ³	lb/ft ³	2.205 x 10 ⁻³
g/ft ³	g/m ³	35.31

Isokinetic Variation.

Calculation from Raw Data.

$$I = \frac{100 T_s [K_3 V_{1c} + (V_m Y / T_m)(P_{bar} + \Delta H / 13.6)]}{60 \theta V_s P_s A_n} \quad \text{Eq. 5-7}$$

where:

$$\begin{aligned} K_3 &= 0.003454 [(\text{mm Hg})(\text{m}^3)]/[(\text{ml})(^\circ\text{K})] \text{ for metric units,} \\ &= 0.002669 [(\text{in. Hg})(\text{ft}^3)]/[(\text{ml})(^\circ\text{R})] \text{ for English units.} \end{aligned}$$

Calculation from Intermediate Values.

$$I = \frac{100 T_s V_{m(\text{std})} P_{\text{std}}}{60 T_{\text{std}} v_s \theta A_n P_s (1 - B_{\text{ws}})} = \frac{K_4 T_s V_{m(\text{std})}}{P_s v_s A_n \theta (1 - B_{\text{ws}})}$$

Eq.5-8

where:

$K_4 = 4.320$ for metric units,

$= 0.09450$ for English units.

Acceptable Results. If 90 percent $\leq I \leq 110$ percent, the results are acceptable. If the PM results are low in comparison to the standard, and "I" is over 110 percent or less than 90 percent, the Administrator may opt to accept the results. Citation 4 in the Bibliography may be used to make acceptability judgments. If "I" is judged to unacceptable, reject the results, and repeat the test.

Average Stack Gas Velocity.

$$v_s = K_p C_p (\sqrt{\Delta p})_{\text{avg}} \sqrt{\frac{T_{s(\text{avg})}}{P_s M_s}}$$

Average Stack Gas Dry Volumetric Flow Rate.

$$Q_{\text{sd}} = 3,600(1 - B_{\text{ws}}) v_s A \frac{T_{\text{std}}}{T_{s(\text{avg})}} \frac{P_s}{P_{\text{std}}}$$

where:

- A = Cross-sectional area of stack, m² (ft²).
- B_{ws} = Water vapor in the gas stream (from Method 5 or Reference Method 4), proportion by volume.
- C_p = Pitot tube coefficient, dimensionless.
- K_p = Pitot tube constant,
- M_d = Molecular weight of stack gas, dry basis (see Section 3.6), g/gmole (lb/lb-mole).
- M_s = Molecular weight of stack gas, wet basis, g/g-mole (lb/lb-mole).

$$= M_d (1 - B_{\text{ws}}) + 18.0 B_{\text{ws}} \quad \text{Eq. 2-5}$$

- P_{bar} = Barometric pressure at measurement site, mm Hg (in. Hg).
- P_g = Stack static pressure, mm Hg (in. Hg).
- P_s = Absolute stack pressure, mm Hg (in. Hg),

$$= P_{\text{bar}} + P_g$$

- P_{std} = Standard absolute pressure, 760 mm Hg (29.92 in. Hg).
- Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, dsm³/hr (dscf/hr).
- t_s = Stack temperature, °C (°F).
- T_s = Absolute stack temperature, °K (°R).

Calibration Certificate for S-Type Pitot Tube

Date: 12-Jan-25 Barometric Pressure ("Hg): 29.78
Pitot I.D.: **200** Wind Tunnel Temperature ($^{\circ}$ F): 70.0
Nozzle: 0.250

Wind Velocity (ft/sec)	Ref.Pitot ("H ₂ O)	S-Type Pitot ("H ₂ O)	Pitot Factor
17.53	0.06982	0.10114	0.82249
41.78	0.39667	0.56684	0.82817
50.67	0.58346	0.81271	0.83883
60.32	0.82699	1.14880	0.83997
86.08	1.68407	2.38761	0.83144
101.99	2.36401	3.27573	0.84102

Average= 0.83365

Note: The new pitot tip should be installed so that the serial number engraved is aligned directly into the gas stream.

Calibrating Technician Signature:



Calibration Certificate for S-Type Pitot Tube

Date: 12-Jan-25 Barometric Pressure ("Hg): 30.05
Pitot I.D.: **140** Wind Tunnel Temperature ($^{\circ}$ F): 70.0
Nozzle: 0.250

Wind Velocity (ft/sec)	Ref.Pitot ("H ₂ O)	S-Type Pitot ("H ₂ O)	Pitot Factor
13.96	0.04470	0.05733	0.87412
19.79	0.08982	0.12082	0.85361
42.36	0.41144	0.58576	0.82971
59.59	0.81441	1.17118	0.82555
80.40	1.48260	2.12088	0.82773
101.66	2.37016	3.46311	0.81901

Average= 0.83829

Note: The new pitot tip should be installed so that the serial number engraved is aligned directly into the gas stream.

Calibrating Technician Signature:



Calibration Certificate for S-Type Pitot Tube

Date: 12-Jan-25 *Barometric Pressure ("Hg):* 29.78
Pitot I.D.: **217** *Wind Tunnel Temperature (°F):* 70.0
Nozzle: 0.250

<i>Wind Velocity (ft/sec)</i>	<i>Ref.Pitot ("H₂O)</i>	<i>S-Type Pitot ("H₂O)</i>	<i>Pitot Factor</i>
13.51	0.04147	0.05467	0.86230
19.93	0.09031	0.12262	0.84962
41.60	0.39339	0.54073	0.84442
62.13	0.87726	1.25293	0.82840
79.94	1.45249	2.09036	0.82524
101.14	2.32467	3.37170	0.82204

Average= 0.83867

Note: The new pitot tip should be installed so that the serial number engraved is aligned directly into the gas stream.

Calibrating Technician Signature:



Calibration Certificate for S-Type Pitot Tube

Date: 12-Jan-25 Barometric Pressure ("Hg): 29.9
Pitot I.D.: **107** Wind Tunnel Temperature ($^{\circ}$ F): 66.0
Nozzle: 0.250

Wind Velocity (ft/sec)	Ref.Pitot ("H ₂ O)	S-Type Pitot ("H ₂ O)	Pitot Factor
11.72	0.03161	0.04242	0.85459
26.28	0.15880	0.22190	0.83748
42.45	0.41433	0.57741	0.83863
58.04	0.77446	1.06033	0.84609
82.87	1.57900	2.18794	0.84102
98.54	2.23250	3.15269	0.83309

Average= 0.84182

Note: The new pitot tip should be installed so that the serial number engraved is aligned directly into the gas stream.

Calibrating Technician Signature:



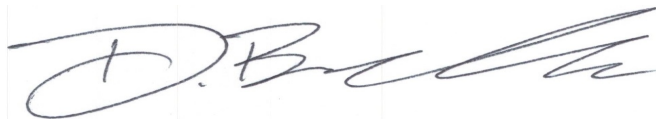
**CALIBRATION CERTIFICATE
DRY GAS METER**

DATE: 13-Jan-25
 CONSOLE MANUF.: NAPP MODEL 31
 CONSOLE I.D.: C-955

PARAMETER SUMMARY	RUN #1	RUN #2	RUN #3
Ta = Ambient (WTM) Temperature (oF.)	68.0	68.0	68.0
P=Pres. Differential at WTM ("Hg)	0.0699	0.0868	0.1766
Pb= Atmospheric Pressure ("Hg)	28.35	28.35	28.35
Pv= Vapour Pressure Water at Temp. Ta ("Hg)	0.6900	0.6900	0.6900
H=Pres. Differential at Orifice	1.0	2.0	3.0
Ti= Dry Test Meter Inlet Temp. (oF.)	80.0	79.0	82.0
To= Dry Test Meter Outlet Temp. (oF.)	68.0	67.0	72.0
Ri= Initial Dry Test volume (ft3)	6.69	99.87	13.53
Rf= Final Dry Test Volume (ft3)	11.54	104.76	18.40
Vi= Initial Wet Test Volume (ft3)	0.0	0.0	0.0
Vf= Final Wet Test Volume (ft3)	5.000	5.000	5.000
Pw= Pb - (^P/13.59) "Hg	28.2801	28.2632	28.1734
Pd= Pb + (^H/13.59) "Hg	28.4236	28.4972	28.5708
Tw= Ta +460 (oR.)	528.0	528.0	528.0
Td= [(Ti + To)/2] + 460 (oR.)	534.0	533.0	537.0
Bw= Pv/Pb ("Hg)	0.0243	0.0243	0.0243
WET TEST METER FACTOR (WTMF)	0.9922	0.9922	0.9922
(Calculated Y Value)(WTMF)	1.0042	0.9910	0.9968
Y (MEAN)(WTMF) =	0.9973		

MCCALL ENVIRONMENTAL

Calibrating Technician Signature:



ORIFICE METER CALIBRATION

DATE: 13-Jan-25

CONSOLE I.D. C-955

	RUN 1	RUN 2	RUN 3
MD= mol. wt. dry air	28.967	28.967	28.967
Pb=bar. pressure "Hg	28.35	28.35	28.35
Y=gas meter factor	1.0042	1.0042	0.9910
Delta H=	0.5	1	1.5
Ri=int. gas meter vol.	21.3	24.1	27.2
Rf=final gas meter vol.	23.17	26.81	30.56
min. samp	5	5	5
$Q_m=Y(R_f-R_i)/\sqrt{T(FT^3/MIN)}$	0.375571	0.544276	0.665952
To=meter outlet Temp (oF)	71	71	72
Tm=meter out temp. (oR)	531	531	532
$P_m=P_b + \Delta H$	28.38679	28.42358	28.46038
$SQRT(T_m/P_m * H/M_d)$	0.568228	0.803075	0.983851
Ko=orifice const.	0.660951	0.67774	0.676883

Ko MEAN : 0.671858

$Ko * 4 * 144 = 386.9903$

McCALL ENVIRONMENTAL LTD.



Calibrating Technician Signature:

ORIFICE METER CALIBRATION

DATE: 13-Jan-25

CONSOLE I.D. C-955

	RUN 4	RUN 5	RUN 6
MD= mol. wt. dry air	28.967	28.967	28.967
Pb=bar. pressure "Hg	28.35	28.35	28.35
Y=gas meter factor	0.991	0.9968	0.9968
Delta H=	2	2.5	3
Ri=int. gas meter vol.	31.1	35.5	40.6
Rf=final gas meter vol.	34.98	39.78	45.3
min. samp	5	5	5
Qm=Y(Rf-Ri)/^T(FT3/MIN)	0.769016	0.853261	0.936992
Tm=meter out temp. (oF)	72	74	74
Tm=meter out temp. (oR.)	532	534	534
Pm=Pb + ^H	28.49717	28.53396	28.57075
SQRT(Tm/Pm*H/Md)	1.13532	1.27089	1.391293
Ko=orifice const.	0.677356	0.671389	0.673468

Ko MEAN : 0.674071

Ko*4*144= 388.2649

McCALL ENVIRONMENTAL LTD.

Calibrating Technician Signature:



**CALIBRATION CERTIFICATE
DRY GAS METER**

DATE: 13-Jan-25

CONSOLE MANUF.: NAPP MODEL 31

CONSOLE I.D.: C-980

PARAMETER SUMMARY	RUN #1	RUN #2	RUN #3
Ta = Ambient (WTM) Temperature (oF.)	69.8	69.8	69.8
P=Pres. Differential at WTM ("Hg)	0.0809	0.1471	0.2060
Pb= Atmospheric Pressure ("Hg)	28.60	28.60	28.60
Pv= Vapour Pressure Water at Temp. Ta ("Hg)	0.7142	0.7142	0.7142
H=Pres. Differential at Orifice	1.0	2.0	3.0
Ti= Dry Test Meter Inlet Temp. (oF.)	88.0	90.0	94.0
To= Dry Test Meter Outlet Temp. (oF.)	77.0	77.0	77.0
Ri= Initial Dry Test volume (ft3)	28.84	21.97	34.72
Rf= Final Dry Test Volume (ft3)	33.73	26.88	39.67
Vi= Initial Wet Test Volume (ft3)	0.0	0.0	0.0
Vf= Final Wet Test Volume (ft3)	5.000	5.000	5.000
Pw= Pb - (^P/13.59) "Hg	28.5191	28.4529	28.3940
Pd= Pb + (^H/13.59) "Hg	28.6736	28.7472	28.8208
Tw= Ta +460 (oR.)	529.8	529.8	529.8
Td= [(Ti + To)/2] + 460 (oR.)	542.5	543.5	545.5
Bw= Pv/Pb ("Hg)	0.0250	0.0250	0.0250
WET TEST METER FACTOR (WTMF)	0.9922	0.9922	0.9922
ated Y Value)(WTMF)	1.0074	1.0003	0.9913
Y (MEAN)(WTMF) =	0.9997		

N.R. MCCALL & ASSOCIATES LTD.

Calibrating Technician Signature:



ORIFICE METER CALIBRATION

DATE: Jan 13 2025

CONSOLE I.D. C-980

	RUN 1	RUN 2	RUN 3
MD= mol. wt. dry air	28.967	28.967	28.967
Pb=bar. pressure "Hg	28.6	28.6	28.6
Y=gas meter factor	1.0074	1.0074	1.0003
Delta H=	0.5	1	1.5
Ri=int. gas meter vol.	45.54	48.3	52
Rf=final gas meter vol.	47.62	51.35	55.7
min. samp	5	5	5
Qm=Y(Rf-Ri)/^T(FT3/MIN)	0.4190784	0.614514	0.740222
To=meter outlet Temp (oF)	77	77	77
Tm=meter out temp. (oR)	537	537	537
Pm=Pb + ^H	28.636792	28.6735835	28.7103753
SQRT(Tm/Pm*H/Md)	0.5689292	0.804071	0.98415064
Ko=orifice const.	0.7366091	0.76425341	0.75214299

Ko MEAN = 0.7510018

Ko*4*144= 432.57705

McCALL ENVIRONMENTAL LTD.



Calibrating Technician Signature:

ORIFICE METER CALIBRATION

DATE: Jan 13 2025

CONSOLE I.D. C-980

	RUN 4	RUN 5	RUN 6
MD= mol. wt. dry air	28.967	28.967	28.967
Pb=bar. pressure "Hg	28.6	28.6	28.6
Y=gas meter factor	1.0003	0.9913	0.9913
Delta H=	2	2.5	3
Ri=int. gas meter vol.	56.3	61.5	66.8
Rf=final gas meter vol.	60.48	66.18	71.9
min. samp	5	5	5
Qm=Y(Rf-Ri)/^T(FT3/MIN)	0.8362508	0.9278568	1.011126
Tm=meter out temp. (oF)	76	77	78
Tm=meter out temp. (oR.)	536	537	538
Pm=Pb + ^H	28.747167	28.783959	28.820751
SQRT(Tm/Pm*H/Md)	1.1346139	1.268908	1.3904243
Ko=orifice const.	0.7370356	0.7312247	0.7272068

Ko MEAN = 0.7318223

Ko*4*144= 421.52966

McCALL ENVIRONMENTAL LTD.

Calibrating Technician Signature:



**CALIBRATION CERTIFICATE
DRY GAS METER**

DATE: 12-Jan-25
 CONSOLE MANUF.: NAPP MODEL 31
 CONSOLE I.D.: C-1021

PARAMETER SUMMARY	RUN #1	RUN #2	RUN #3
Ta = Ambient (WTM) Temperature (oF.)	69.8	69.8	69.8
P=Pres. Differential at WTM ("Hg)	0.0691	0.1250	0.1839
Pb= Atmospheric Pressure ("Hg)	28.60	28.60	28.60
Pv= Vapour Pressure Water at Temp. Ta ("Hg)	0.7142	0.7142	0.7142
H=Pres. Differential at Orifice	1.0	2.0	3.0
Ti= Dry Test Meter Inlet Temp. (oF.)	82.0	81.0	84.0
To= Dry Test Meter Outlet Temp. (oF.)	75.0	75.0	76.0
Ri= Initial Dry Test volume (ft3)	63.95	57.10	69.85
Rf= Final Dry Test Volume (ft3)	68.83	61.98	74.75
Vi= Initial Wet Test Volume (ft3)	0.0	0.0	0.0
Vf= Final Wet Test Volume (ft3)	5.000	5.000	5.000
Pw= Pb - (^P/13.59) "Hg	28.5309	28.4750	28.4161
Pd= Pb + (^H/13.59) "Hg	28.6736	28.7472	28.8208
Tw= Ta +460 (oR.)	529.8	529.8	529.8
Td= [(Ti + To)/2] + 460 (oR.)	538.5	538.0	540.0
Bw= Pv/Pb ("Hg)	0.0250	0.0250	0.0250
WET TEST METER FACTOR (WTMF)	0.9922	0.9922	0.9922
(Calculated Y Value)(WTMF)	1.0025	0.9970	0.9920
Y (MEAN)(WTMF) =	0.9972		

MCCALL ENVIRONMENTAL

Calibrating Technician Signature:



ORIFICE METER CALIBRATION

DATE: 12-Jan-25

CONSOLE I.D. C-1021

	RUN 1	RUN 2	RUN 3
MD= mol. wt. dry air	28.967	28.967	28.967
Pb=bar. pressure "Hg	28.6	28.6	28.6
Y=gas meter factor	1.0025	1.0025	0.9970
Delta H=	0.5	1	1.5
Ri=int. gas meter vol.	75.6	85.6	88.33
Rf=final gas meter vol.	77.5	88.26	91.64
min. samp	5	5	5
Qm=Y(Rf-Ri)/^T(FT3/MIN)	0.38095	0.53333	0.660014
To=meter outlet Temp (oF)	75	75	77
Tm=meter out temp. (oR)	535	535	537
Pm=Pb + ^H	28.636792	28.673584	28.710375
SQRT(Tm/Pm*H/Md)	0.5678687	0.8025723	0.9841506
Ko=orifice const.	0.6708417	0.6645258	0.6706433

Ko MEAN = 0.6686703

Ko*4*144= 385.15407

McCALL ENVIRONMENTAL LTD.



Calibrating Technician Signature:

ORIFICE METER CALIBRATION

DATE: 12-Jan-25

CONSOLE I.D. C-1021

	RUN 4	RUN 5	RUN 6
MD= mol. wt. dry air	28.967	28.967	28.967
Pb=bar. pressure "Hg	28.6	28.6	28.6
Y=gas meter factor	0.997	0.9920	0.9920
Delta H=	2	2.5	3
Ri=int. gas meter vol.	95.91	99.8	104.2
Rf=final gas meter vol.	99.72	104.11	108.97
min. samp	5	5	5
$Q_m = Y(R_f - R_i) / \sqrt{T(FT^3/MIN)}$	0.759714	0.855104	0.946368
To=meter outlet Temp (oF)	77	78	78
Tm=meter out temp. (oR)	537	538	538
$P_m = P_b + \Delta H$	28.747167	28.783959	28.820751
$SQRT(T_m / P_m * H / M_d)$	1.1356718	1.2700889	1.3904243
Ko=orifice const.	0.6689556	0.6732631	0.6806325

Ko MEAN = 0.6742837

$Ko * 4 * 144 = 388.38743$

McCALL ENVIRONMENTAL LTD.



Calibrating Technician Signature:

**CALIBRATION CERTIFICATE
DRY GAS METER**

DATE: 13-Jan-25

CONSOLE MANUF.: NAPP MODEL 31

CONSOLE I.D.: C-1039

PARAMETER SUMMARY	RUN #1	RUN #2	RUN #3
Ta = Ambient (WTM) Temperature (oF.)	69.8	69.8	69.8
P=Pres. Differential at WTM ("Hg)	0.0883	0.1618	0.2428
Pb= Atmospheric Pressure ("Hg)	28.35	28.35	28.35
Pv= Vapour Pressure Water at Temp. Ta ("Hg)	0.7142	0.7142	0.7142
H=Pres. Differential at Orifice	1.0	2.0	3.0
Ti= Dry Test Meter Inlet Temp. (oF.)	96.0	98.0	104.0
To= Dry Test Meter Outlet Temp. (oF.)	81.0	77.0	85.0
Ri= Initial Dry Test volume (ft3)	69.98	63.92	78.89
Rf= Final Dry Test Volume (ft3)	74.83	68.88	83.92
Vi= Initial Wet Test Volume (ft3)	0.0	0.0	0.0
Vf= Final Wet Test Volume (ft3)	5.000	5.000	5.000
Pw= Pb - (^P/13.59) "Hg	28.2617	28.1882	28.1072
Pd= Pb + (^H/13.59) "Hg	28.4236	28.4972	28.5708
Tw= Ta +460 (oR.)	529.8	529.8	529.8
Td= [(Ti + To)/2] + 460 (oR.)	548.5	547.5	554.5
Bw= Pv/Pb ("Hg)	0.0252	0.0252	0.0252
WET TEST METER FACTOR (WTMF)	0.9922	0.9922	0.9922
ated Y Value)(WTMF)	1.0264	0.9967	0.9899

Y (MEAN)(WTMF) = 1.0043

MCCALL ENVIRONMENTAL

Calibrating Technician Signature:



ORIFICE METER CALIBRATION

DATE: 13-Jan-25

CONSOLE I.D. C-1039

	RUN 1	RUN 2	RUN 3
MD= mol. wt. dry air	28.967	28.967	28.967
Pb=bar. pressure "Hg	28.35	28.35	28.35
Y=gas meter factor	1.0264	1.0264	0.9967
Delta H=	0.5	1	1.5
Ri=int. gas meter vol.	85.1	87.7	91.5
Rf=final gas meter vol.	87.38	90.93	95.43
min. samp	5	5	5
$Q_m=Y(R_f-R_i)/^T(FT^3/MIN)$	0.4680384	0.6630544	0.7834062
Tm=meter out temp. (oF)	86	87	89
Tm=meter out temp. (oR.)	546	547	549
$P_m=P_b + ^H$	28.386792	28.423584	28.460375
$SQRT(T_m/P_m*H/M_d)$	0.5761976	0.8150842	0.9994469
Ko=orifice const.	0.8122881	0.8134796	0.7838397

Ko MEAN = 0.8032025

$K_o^4 * 144 = 462.64462$

McCALL ENVIRONMENTAL



Calibrating Technician Signature:

ORIFICE METER CALIBRATION

DATE: 13-Jan-25

CONSOLE I.D. C-1039

	RUN 4	RUN 5	RUN 6
MD= mol. wt. dry air	28.967	28.967	28.967
Pb=bar. pressure "Hg	28.35	28.35	28.35
Y=gas meter factor	0.9967	0.9899	0.9899
Delta H=	2	2.5	3
Ri=int. gas meter vol.	95.8	101.1	106.6
Rf=final gas meter vol.	100.32	106.17	112.16
min. samp	5	5	5
$Q_m=Y(R_f-R_i)/^T(FT^3/MIN)$	0.9010168	1.0037586	1.1007688
Tm=meter out temp. (oF)	89	89	90
Tm=meter out temp. (oR.)	549	549	550
$P_m=P_b + ^H$	28.497167	28.533959	28.570751
$SQRT(T_m/P_m*H/M_d)$	1.1533167	1.2886157	1.4119827
Ko=orifice const.	0.7812397	0.7789434	0.7795908

Ko MEAN = 0.7799246

$Ko^4*144=$ 449.23659

McCALL ENVIRONMENTAL



Calibrating Technician Signature:



Smithers Pellet Limited Partnership

Production rate during stack test (Feb 13, 2025)

13.4 MT/hr

Average for the previous calendar month

12.3 MT/hr

90th percentile production rate

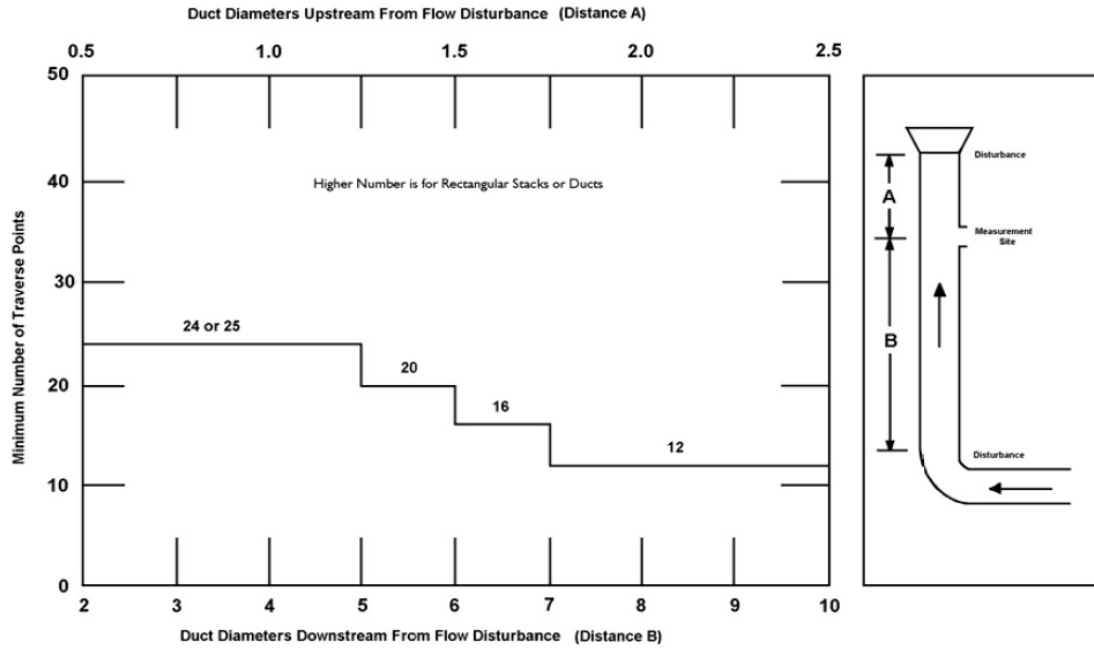
14.9 MT/hr

Average hourly dryer exit temperature during testing:

Included in report



Site Diagram & Sample Point Selection



Client: Pinnacle Pellet Smithers
 Source: Dryer Stackls 1-4
 Pollution Abatement Equipment:
 Duct Diameters Up (A): >2
 Duct Diameters Down (B): 4
 Area of Stack (ft): 33.18
 Stack Diameter (in): 78
 Zero (in): 4
 Number of Points: 24

Traverse Points (in):
 PT-1 1.64
 PT-2 5.22
 PT-3 9.21
 PT-4 13.8
 PT-5 19.5
 PT-6 27.69
 PT-7 50.31
 PT-8 58.5
 PT-9 64.19
 PT-10 68.8
 PT-11 70.7
 PT-12 76.36

Cyclonic Angle: 5°

Analytical Report

Bill To: McCall Environmental 6733 Buchanan Road Coldstream, BC, Canada V1B 3C5	Project ID: Project Name: Drax Smithers Project Location: LSD: P.O.:	Lot ID: 1795228 Control Number: Date Received: Feb 18, 2025 Date Reported: Feb 19, 2025 Report Number: 3107302 Report Type: Final Report
Attn: Accounts Payable Sampled By: Company: McCall	Proj. Acct. code:	


Reference Number	1795228-1	1795228-2	1795228-3
Sample Date	Feb 13, 2025	Feb 13, 2025	Feb 13, 2025
Sample Time	NA	NA	NA
Sample Location			
Sample Description	Dryer Stack 1 Test 1 / 9.5 °C / Filter: P96	Dryer Stack 1 Test 2 / 9.5 °C / Filter: P97	Dryer Stack 1 Test 3 / 9.5 °C / Filter: P98
Matrix	Water	Water	Water

Analyte	Units	Results	Results	Results	Nominal Detection Limit
Aggregate Organic Constituents					
Oil and Grease	Total	mg/sample	<2	<2	<2
Volume	Sample volume	mL	254	279	285
pH adjustment	required prior to O&G extraction		Yes	Yes	Yes

Analytical Report

Bill To: McCall Environmental 6733 Buchanan Road Coldstream, BC, Canada V1B 3C5	Project ID: Project Name: Drax Smithers Project Location: LSD: P.O.:	Lot ID: 1795228 Control Number: Date Received: Feb 18, 2025 Date Reported: Feb 19, 2025 Report Number: 3107302 Report Type: Final Report
Attn: Accounts Payable	Proj. Acct. code:	
Sampled By:		
Company: McCall		

	Reference Number	1795228-4	1795228-5	1795228-6	
	Sample Date	Feb 13, 2025	Feb 13, 2025	Feb 13, 2025	
	Sample Time	NA	NA	NA	
	Sample Location				
	Sample Description	Dryer Stack 2 Test 1 / 9.5 °C / Filter: P93	Dryer Stack 2 Test 2 / 9.5 °C / Filter: P94	Dryer Stack 2 Test 3 / 9.5 °C / Filter: P95	
	Matrix	Water	Water	Water	
Analyte	Units	Results	Results	Results	Nominal Detection Limit
Aggregate Organic Constituents					
Oil and Grease	Total	mg/sample	<2	<2	2
Volume	Sample volume	mL	294	302	264
pH adjustment	required prior to O&G extraction	Yes	Yes	Yes	

Approved by: 
 Rachel Eden, B. Sc.
 Operations Manager

Methodology and Notes

Bill To: McCall Environmental 6733 Buchanan Road Coldstream, BC, Canada V1B 3C5	Project ID: Project Name: Drax Smithers Project Location: LSD: P.O.:	Lot ID: 1795228 Control Number: Date Received: Feb 18, 2025 Date Reported: Feb 19, 2025 Report Number: 3107302 Report Type: Final Report
Attn: Accounts Payable Sampled By: Company: McCall	Proj. Acct. code:	

Method of Analysis

Method Name	Reference	Method	Date Analysis Started	Location
Oil and Grease in water (VAN)	BCELM	* Oil & Grease in Water - Direct Hexane Extraction (2023), Oil & Grease <i>* Reference Method Modified</i>	Feb 18, 2025	Element Vancouver

References

BCELM B.C. Environmental Laboratory Manual

Please direct any inquiries regarding this report to our Client Services group.
 Results relate only to samples as submitted.

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Analytical Report

Bill To: McCall Environmental 6733 Buchanan Road Coldstream, BC, Canada V1B 3C5	Project ID: Project Name: Drax Smithers Project Location: LSD: P.O.:	Lot ID: 1795230 Control Number: Date Received: Feb 18, 2025 Date Reported: Feb 19, 2025 Report Number: 3107304 Report Type: Final Report
Attn: Accounts Payable Sampled By: Company: McCall	Proj. Acct. code:	

Reference Number	1795230-1	1795230-2	1795230-3
Sample Date	Feb 14, 2025	Feb 14, 2025	Feb 14, 2025
Sample Time	NA	NA	NA
Sample Location			
Sample Description	Dryer Stack 3 Test 1 / 9.8 °C / Filter: Q2	Dryer Stack 3 Test 2 / 9.8 °C / Filter: Q3	Dryer Stack 3 Test 3 / 9.8 °C / Filter: Q4
Matrix	Water	Water	Water

Analyte	Units	Results	Results	Results	Nominal Detection Limit
Aggregate Organic Constituents					
Oil and Grease	Total	mg/sample	3	3	<2
Volume	Sample volume	mL	310	304	321
pH adjustment	required prior to O&G extraction		Yes	Yes	Yes

Analytical Report

Bill To: McCall Environmental 6733 Buchanan Road Coldstream, BC, Canada V1B 3C5	Project ID: Project Name: Drax Smithers Project Location: LSD: P.O.:	Lot ID: 1795230 Control Number: Date Received: Feb 18, 2025 Date Reported: Feb 19, 2025 Report Number: 3107304 Report Type: Final Report
Attn: Accounts Payable	Proj. Acct. code:	
Sampled By:		
Company: McCall		


	Reference Number	1795230-4	1795230-5	1795230-6	
	Sample Date	Feb 14, 2025	Feb 14, 2025	Feb 14, 2025	
	Sample Time	NA	NA	NA	
	Sample Location				
	Sample Description	Dryer Stack 4 Test 1 / 9.8 °C / Filter: Q5	Dryer Stack 4 Test 2 / 9.8 °C / Filter: Q6	Dryer Stack 4 Test 3 / 9.8 °C / Filter: Q7	
	Matrix	Water	Water	Water	
Analyte	Units	Results	Results	Results	Nominal Detection Limit
Aggregate Organic Constituents					
Oil and Grease	Total	mg/sample	2	3	4
Volume	Sample volume	mL	289	309	300
pH adjustment	required prior to O&G extraction		Yes	Yes	Yes

Analytical Report

Bill To: McCall Environmental 6733 Buchanan Road Coldstream, BC, Canada V1B 3C5	Project ID: Project Name: Drax Smithers Project Location: LSD: P.O.:	Lot ID: 1795230 Control Number: Date Received: Feb 18, 2025 Date Reported: Feb 19, 2025 Report Number: 3107304 Report Type: Final Report
Attn: Accounts Payable Sampled By: Company: McCall	Proj. Acct. code:	

Reference Number 1795230-7
Sample Date Feb 14, 2025
Sample Time NA
Sample Location
Sample Description Blank Water / 9.8 °C / Blank H2O
Matrix Water

Analyte	Units	Results	Results	Results	Nominal Detection Limit
Aggregate Organic Constituents					
Oil and Grease	Total	mg/sample	<2		2
Volume	Sample volume	mL	294		
pH adjustment	required prior to O&G extraction		Yes		

Approved by: 
 Rachel Eden, B. Sc.
 Operations Manager

Methodology and Notes

Bill To: McCall Environmental 6733 Buchanan Road Coldstream, BC, Canada V1B 3C5	Project ID: Project Name: Drax Smithers Project Location: LSD: P.O.:	Lot ID: 1795230 Control Number: Date Received: Feb 18, 2025 Date Reported: Feb 19, 2025 Report Number: 3107304 Report Type: Final Report
Attn: Accounts Payable Sampled By: Company: McCall	Proj. Acct. code:	

Method of Analysis

Method Name	Reference	Method	Date Analysis Started	Location
Oil and Grease in water (VAN)	BCELM	* Oil & Grease in Water - Direct Hexane Extraction (2023), Oil & Grease	Feb 18, 2025	Element Vancouver
Oil and Grease in water (VAN)	BCELM	* Oil & Grease in Water - Direct Hexane Extraction (2023), Oil & Grease	Feb 18, 2025	Element Vancouver

** Reference Method Modified*

References

BCELM B.C. Environmental Laboratory Manual

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Client Name: Dray
Smithers
 Process: Dryer Stack 1
 Test Number: 1 - COND.
 Date: FEB 13/25
 Start Time: 1046
 Finish Time: 1148
 Starting Vol.: 300
 Final Vol.: 303
 Flask: P-916
 Console: 980
 Stack Diameter: 6.5 ft

BP 28.15
 DN .277
 CP .83365
 MF .9997
 Moist. 2%
 PM 28.26
 AS
 Ko .7510
 Pitot 200
 Port
 Static -.20
 PS 28.14

CO ₂	O ₂	CO	N ₂
0	20.9		
0	20.9		
0	20.9		
0	20.9		

Duct Diameters
Up-Stream

Duct Diameters
Downstream

Personnel: DL CB

Mean Yaw Angle

Leakage Rate @ 15 inches Start: .006 Finish: .009

Load:

.27-.38

90

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A12	.27	1.38	33	33	64	2.96	1	270	1000	
11	.26	1.43	63	54	56	4.81				
10	.28	1.53	72	55	65	6.61				
9	.27	1.48	74	57	65	8.49				
8	.27	1.48	69	55	62	10.40				
7	.30	1.65	80	58	65	12.30				
6	.30	1.65	74	57	63	14.11	1			
5	.29	1.60	77	59	64	15.96				
4	.29	1.60	79	63	66	17.77				
3	.28	1.55	81	64	65	19.68				
2	.27	1.50	83	64	65	21.48				
1	.27	1.47	65	64	68	23.12				
B12	.29	1.31	73	62	68	25.04	1			
11	.25	1.37	76	62	68	26.65				
10	.26	1.42	74	62	67	28.34				
9	.27	1.49	78	63	66	30.04				
8	.28	1.55	81	66	67	31.90				
7	.27	1.49	84	65	69	33.65				
6	.29	1.62	84	70	65	35.39	1			
5	.30	1.69	88	72	65	37.36				
4	.29	1.64	88	73	64	39.32				
3	.28	1.58	89	75	64	41.28				
2	.27	1.53	90	74	64	43.08				
1	.26	1.46	91	74	65	44.94				
						46.71				

Client Name: Dray Smithers
 Process: Dryer Stack 1
 Test Number: 2
 Date: Feb 13 2025
 Start Time: 1221
 Finish Time: 123
 Starting Vol.: 300
 Final Vol.: 304
 Flask: P97
 Console:
 Stack Diameter: 6.5 ft

BP 28.15
 DN .277
 CP .83365
 MF .9997
 Moist. 10%
 PM 28.26
 AS
 Ko 0.7510
 Pitot 200
 Port
 Static -.20
 PS 28.14

CO ₂	O ₂	CO	N ₂
0	20.9		
0	20.9		
0	20.9		
0	20.9		

Duct Diameters
 Up-Stream

Duct Diameters
 Downstream

Personnel: CB CB

Mean Yaw Angle

Leakage Rate @ 15 inches

Start: .008 Finish: 017

Load:

90

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A12	.25	1.40	69	73	66	46.84	0	27.0	Ice	
11	.26	1.47	74	70	64	48.65				
10	.28	1.58	79	70	65	50.46				
9	.27	1.54	87	72	65	52.24				
8	.27	1.54	84	71	63	54.02				
7	.29	1.66	91	73	65	55.82	1			
6	.30	1.73	91	79	64	57.69				
5	.30	1.73	93	75	65	59.66				
4	.28	1.62	94	75	64	61.68				
3	.28	1.62	94	76	64	63.40				
2	.27	1.56	97	77	67	65.20				
1	.27	1.57	96	80	64	67.21				
B12	0.25	1.46	99	81	65	69.20	2			
11	0.25	1.45	97	79	64	70.99				
10	0.26	1.52	101	83	65	72.72				
9	0.27	1.58	101	82	64	74.45				
8	0.26	1.58	102	84	64	76.39				
7	0.29	1.70	102	85	64	78.27				
6	0.29	1.70	103	85	65	80.27	2			
5	.30	1.76	103	86	65	82.14				
4	.29	1.71	105	86	65	84.14				
3	0.28	1.65	105	87	66	86.23				
2	0.27	1.59	104	88	65	88.28				
1	0.25	1.47	105	89	64	90.17				
						91.99				

Client Name: Draft Smithers
 Process: Dryer Stack 1
 Test Number: 5
 Date: Feb 13 2025
 Start Time: 200
 Finish Time: 302
 Starting Vol.: 300
 Final Vol.: 304
 Flask: 298
 Console: 980
 Stack Diameter: 6.5 F1

BP 28.15
 DN 0.277
 CP 2.83365
 MF 0.0997
 Moist. 1%
 PM 28.26
 AS ~
 Ko 0.7510
 Pitot 200
 Port ~
 Static -.20
 PS 28.14

CO ₂	O ₂	CO	N ₂
0	20.9		
0	20.9		
0	20.9		
0	20.9		

Duct Diameters
 Up-Stream
 Duct Diameters
 Downstream
 Mean Yaw Angle

Personnel: AK/CS

Leakage Rate @ 15 inches

Start: 0.04 Finish: 0.06

Load:

83

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A12	.24	1.28	44	45	67	92.34	2	270	100	
11	.26	1.39	46	44	67	94.09				
10	.29	1.54	49	43	68	95.87				
9	.28	1.50	51	44	68	97.75				
8	.27	1.45	52	44	69	99.63				
7	.30	1.61	53	45	69	101.48				
6	.30	1.62	55	45	66	103.29	3			
5	.29	1.57	56	46	66	105.06				
4	.28	1.51	57	46	67	106.91				
3	.27	1.46	58	47	68	108.68				
2	.26	1.40	59	47	69	110.49				
1	.26	1.41	59	48	68	112.35				
B12	.25	1.35	58	49	68	114.20	2			
11	.26	1.41	59	48	67	115.96				
10	.26	1.41	60	49	67	117.83				
9	.28	1.52	61	50	68	119.60				
8	.29	1.57	62	50	68	121.43				
7	.29	1.58	63	51	69	123.22				
6	.30	1.64	65	52	68	125.01	2			
5	.29	1.59	67	53	68	126.89				
4	.28	1.54	70	54	67	128.72				
3	.27	1.49	72	55	67	130.51				
2	.26	1.44	73	55	66	132.36				
1	.25	1.39	73	56	66	134.10				
						135.88				

Client Name: DRAK
 Process: DRYER ST. 2
 Test Number: 1-CONO
 Date: FEB 13/25
 Start Time: 10:46
 Finish Time: 11:48
 Starting Vol.: 300
 Final Vol.: 305
 Flask: P-93
 Console: 1021
 Stack Diameter: _____

BP 28.15
 DN 275
 CP 84182
 MF 9972
 Moist: .02
 PM 28.26
 AS .6686
 Ko 0.6686
 Pitot 107
 Port _____
 Static -0.19
 PS 28.13

CO ₂	O ₂	CO	N ₂
0	20.9	0	

Duct Diameters
 Up-Stream _____
 Duct Diameters
 Downstream _____
 Mean Yaw Angle _____

Personnel: CS/CS

Leakage Rate @ 15 inches _____ Start: 0:05 Finish: 0:07

Load: _____

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A-12	0.28	1.88	61	51	69	39.12	1	270	1000	0
11	0.36	2.38	64	63	81	41.00				2.5
10	0.26	1.70	57	51	72	42.90				5
9	0.28	1.73	60	52	81	44.65				7.5
8	0.25	1.63	61	53	81	46.43				10
7	0.25	1.67	80	55	81	48.11				12.5
6	0.24	1.58	68	57	81	49.72	1			15
5	0.21	1.52	69	61	82	51.41				17.5
4	0.21	1.33	74	58	82	53.07				20
3	0.20	1.32	69	60	82	54.61				22.5
2	0.17	1.12	69	60	82	56.13				25
1	0.16	1.04	66	64	88	57.42				27.5
B-12	0.27	1.77	67	55	86	58.87	1			30
11	0.32	2.11	70	65	85	60.52				32.5
10	0.27	1.79	73	65	83	62.36				35
9	0.28	1.87	73	66	80	64.15				37.5
8	0.26	1.74	75	67	82	66.09				40
7	0.25	1.67	75	67	81	67.79				42.5
6	0.23	1.54	76	69	82	69.53	1			45
5	0.23	1.54	77	69	81	71.23				47.5
4	0.20	1.34	76	70	82	72.94				50
3	0.21	1.41	77	72	81	74.59				52.5
2	0.17	1.14	77	71	83	76.17				55
1	0.16	1.15	76	71	83	77.74				57.5
						79.20	1			60

Client Name: Prax
Smitos
 Process: Dryer stack 2
 Test Number: 2
 Date: Feb. 11/2023
 Start Time: 12:24pm
 Finish Time: 1:23
 Starting Vol.: 300
 Final Vol.: 305
 Flask: P 94
 Console: 1021
 Stack Diameter: _____

BP 28.15
 DN 0.275
 CP 0.84182
 MF 0.9972
 Moist. 1.9%
 PM 28.26
 AS ~
 Ke 0.6686
 Pitot 107
 Port ~
 Static -0.19
 PS 28.13

CO ₂	O ₂	CO	N ₂
0	20.9		

Duct Diameters
Up-Stream

 Duct Diameters
Downstream

 Mean Yaw Angle

Personnel: B/C/S

Leakage Rate @ 15 inches

Start: 0.04 Finish: 0.06

Load:

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A 12	1.129	1.97	70	72	84	79.85	0	270	Iced	0
11	0.30	2.04	76	71	83	81.77				2.5
10	0.18	1.77	75	71	82	83.60				5
9	0.27	1.85	77	72	81	85.35				7.5
8	0.26	1.78	79	72	83	87.27				10
7	0.25	1.71	80	73	83	88.97				12.5
6	0.23	1.58	82	74	83	90.93				15
5	0.23	1.58	82	75	83	92.49				17.5
4	0.20	1.39	85	86	82	94.33	0			20
3	0.20	1.40	85	87	82	96.06				22.5
2	0.18	1.25	87	78	82	97.68				25
1	0.16	1.11	88	81	83	99.10				27.5
B 12	0.28	1.95	89	82	83	100.57				30
11	0.23	2.30	89	82	83	102.38				32.5
10	0.29	2.02	90	81	83	104.50				35
9	0.28	1.96	94	85	83	106.52				37.5
8	0.26	1.82	95	85	84	108.40	0			40
7	0.25	1.76	95	87	83	110.37				42.5
6	0.22	1.55	96	88	83	112.14				45
5	0.22	1.56	96	89	83	113.85				47.5
4	0.20	1.41	95	89	83	115.78				50
3	0.22	1.55	97	90	85	117.01				52.5
2	0.17	1.20	97	91	84	118.88				55
1	0.15	1.06	98	92	84	120.35	0			57.5
						121.85				60

Client Name: Drax
Smelters
 Process: Dryer Stack 2
 Test Number: 3
 Date: Feb 13/2025
 Start Time: 200
 Finish Time: 302
 Starting Vol.: 300
 Final Vol.: 305
 Flask: P95
 Console: 1021
 Stack Diameter: _____

BP 28.15
 DN 0.275
 CP 0.18482
 MF 0.9972
 Moist. 1%
 PM 28.26
 AS ~
 Ko 0.6686
 Pitot 107
 Port -
 Static -0.19
 PS 28.13

CO ₂	O ₂	CO	N ₂
0	20.9		
0	20.9		
0	20.9		
0	20.9		

Duct Diameters
 Up-Stream _____
 Duct Diameters
 Downstream _____
 Mean Yaw Angle _____

Personnel: CB CB

Leakage Rate @ 15 inches _____

Start: 1012 Finish: 1014

Load: _____

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A12	0.20	1.98	55	54	82	27.14	1	270	iced	
11	0.24	1.92	57	53	81	24.04				
10	0.27	1.79	58	53	80	25.90				
9	0.26	1.72	59	52	80	27.72				
8	0.26	1.72	60	52	79	29.49				
7	0.25	1.66	61	52	79	31.26				
6	0.23	1.54	62	53	78	33.01	1			
5	0.22	1.53	62	53	79	34.71				
4	0.20	1.33	63	54	80	36.52				
3	0.21	1.40	63	54	80	38.21				
2	0.18	1.21	64	55	79	39.81				
1	0.16	1.07	65	55	78	41.34				
B12	0.28	1.88	65	56	78	42.78	1			
11	0.33	2.22	66	56	77	44.63				
10	0.30	2.02	67	57	78	46.57				
9	0.28	1.89	68	57	78	48.48				
8	0.26	1.75	69	58	79	50.31				
7	0.25	1.69	69	58	79	52.10				
6	0.22	1.48	70	59	80	53.93	1			
5	0.22	1.49	71	60	80	55.67				
4	0.19	1.28	72	61	81	57.42				
3	0.20	1.36	73	62	80	58.94				
2	0.16	1.09	73	63	79	60.61				
1	0.15	1.02	74	63	78	62.04				
						63.46				

Client Name: DRAY
 Process: DRAYER ST. 3
 Test Number: 1
 Date: FEB 13/25
 Start Time: 11:10
 Finish Time: 12:12
 Starting Vol.: 300
 Final Vol.: 314
 Flask: Q-2
 Console: 955
 Stack Diameter: _____

BP 28.15
 DN 270
 CP 83867
 MF 19973
 Moist. .02
 PM 28.24
 AS _____
 Ko 1.6718
 Pitot 217
 Port _____
 Static -1.23
 PS 28.13

CO ₂	O ₂	CO	N ₂

Duct Diameters
Up-Stream

 Duct Diameters
Downstream

 Mean Yaw Angle

 Leakage Rate @ 15 inches
 Start: 1007 Finish: 1009

Personnel: DL/DB
 Load: _____

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A-12	.23	1.31	21	21	68	55.93	1	250	1009	
11	.23	1.30	38	23	80	57.30				
10	.24	1.37	41	25	81	58.65				
9	.25	1.42	40	26	81	60.10	1			
8	.23	1.31	42	29	82	61.57				
7	.24	1.38	44	33	81	63.00				
6	.25	1.45	48	34	81	64.50	1			
5	.27	1.56	53	35	80	66.00				
4	.29	1.70	58	39	80	67.70				
3	.30	1.77	62	40	80	69.50	1			
2	.30	1.78	67	46	83	71.24				
1	.27	1.62	72	49	82	73.03				
B-12	.24	1.45	75	51	79	74.70	1			
11	.24	1.45	81	54	80	76.35				
10	.25	1.51	82	56	82	78.02				
9	.24	1.47	84	58	82	79.61	1			
8	.23	1.41	88	62	80	81.25				
7	.24	1.48	90	63	81	82.85				
6	.24	1.49	92	66	81	84.50				
5	.26	1.62	93	67	86	86.20	1			
4	.27	1.68	94	69	81	87.85				
3	.29	1.82	96	71	81	89.60				
2	.30	1.88	96	73	81	91.43	1			
1	.30	1.88	97	74	81	93.33				
						95.23				

Client Name: DIAX

Process: DRYER ST 3

Test Number: 2-COND

Date: FEB 13/25

Start Time: 12:45

Finish Time: 1:48

Starting Vol.: 300

Final Vol.: 310

Flask: Q-3

Console: 953

Stack Diameter

BP 28.15

DN 1.270

CP 83867

MF 9973

Moist. .02

PM 28.26

AS

Ko .6718

Pitot 217

Port

Static -.23

PS 28.13

CO ₂	O ₂	CO	N ₂

Duct Diameters

Up-Stream

Duct Diameters

Downstream

Personnel:

Mean Yaw Angle

Leakage Rate @ 15 inches

Start: .01 Finish: .01

Load:

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A-12	.24	1.47	71	71	82	95.90		270	(ICE)	
11	.24	1.48	79	70	81	97.56				
10	.25	1.54	80	70	82	99.25				
9	.26	1.62	87	72	82	100.85				
8	.26	1.63	88	85	80	102.70				
7	.27	1.69	91	77	83	104.50				
6	.26	1.63	93	78	81	106.26				
5	.28	1.75	94	79	82	108.13				
4	.29	1.83	95	81	82	109.90				
3	.30	1.90	96	83	82	111.80				
2	.28	1.77	97	85	83	113.65				
1	.29	1.85	101	84	81	115.40				
B-12	.25	1.59	103	85	84	117.40				
11	.25	1.59	104	86	84	119.14				
10	.27	1.72	108	88	83	120.94				
9	.25	1.61	110	91	84	122.75				
8	.25	1.61	111	93	85	124.60				
7	.26	1.68	112	96	86	126.50				
6	.26	1.68	110	95	85	128.23				
5	.28	1.80	110	96	86	130.07				
4	.29	1.86	111	95	89	131.90				
3	.30	1.92	112	96	86	133.92				
2	.28	1.79	112	95	85	135.90				
1	.28	1.79	112	95	86	137.81				
						139.70		40270	40160	

Client Name: DRAY
 Process: DRYER ST. 3
 Test Number: 3 - COND
 Date: FEB 13/25
 Start Time: 2:20
 Finish Time: 3:23
 Starting Vol.: 300
 Final Vol.: 313
 Flask: Q-4
 Console: 955
 Stack Diameter: _____

BP 28.15
 DN 270
 CP 83867
 MF 9973
 Moist. 102
 PM 28.26
 AS _____
 Ko 1.6718
 Pitot 217
 Port _____
 Static -123
 PS 28.13

CO ₂	O ₂	CO	N ₂

Duct Diameters
Up-Stream

 Duct Diameters
Downstream

Personnel: _____

Mean Yaw Angle

Leakage Rate @ 15 inches

Start: 02 Finish: .01

Load:

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A-12	.24	1.42	55	56	83	41.70	0	270	ICEID	
11	.24	1.45	60	59	78	43.43				
10	.25	1.51	62	60	78	44.95	1			
9	.26	1.57	63	61	80	46.70				
8	.26	1.57	68	62	79	48.36				
7	.27	1.65	75	62	80	50.00				
6	.27	1.67	82	64	79	51.66				
5	.27	1.67	85	66	79	53.40				
4	.28	1.75	90	68	77	55.14				
3	.29	1.83	93	69	75	56.90				
2	.30	1.89	93	70	77	58.78	1			
1	.30	1.90	96	73	78	60.75	2			
B-12	.23	1.45	99	75	78	62.60				
11	.23	1.45	101	78	78	64.30				
10	.25	1.58	101	78	78	65.95				
9	.26	1.67	103	82	77	67.70				
8	.26	1.67	105	83	78	69.50				
7	.27	1.73	105	84	77	71.30	2			
6	.28	1.81	106	86	76	73.10				
5	.28	1.81	109	87	78	75.03				
4	.30	1.94	109	88	76	76.94				
3	.29	1.88	110	89	77	78.90				
2	.29	1.88	108	86	76	80.82				
1	.28	1.82	108	86	75	82.80	2	270	ICEID	
						84.70				

Client Name: DRYER
 Process: DRYER ST.4
 Test Number: 1-COND
 Date: FEB 13/25
 Start Time: 11:41
 Finish Time: 12:13
 Starting Vol.: 300
 Final Vol.: 307
 Flask: Q-5
 Console: 1039
 Stack Diameter: _____

BP 28.15
 DN .270
 CP .83829
 MF 1.0043
 Moist. .02
 PM 28.26
 AS _____
 Ko .8032
 Pitot 140
 Port _____
 Static -.16
 PS .28.15

CO ₂	O ₂	CO	N ₂
0	21		

Duct Diameters
 Up-Stream _____
 Duct Diameters
 Downstream _____
 Mean Yaw Angle _____

Personnel: JTB
 Leakage Rate @ 15 inches _____

Start: .003 Finish: .001

Load: _____

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
17	.26	1.00	40	40	96	30.01	0	270	1125	
11	.28	1.11	48	40	93	31.92				
10	.24	.96	52	40	93	33.20	1			
9	.18	.72	58	42	93	34.81				
8	.16	.65	64	43	92	36.11				
7	.16	.65	69	45	93	37.36				
6	.16	.66	73	46	92	38.64				
5	.17	.70	79	50	93	39.92				
4	.24	1.00	83	52	95	41.30	1			
3	.26	1.10	87	54	96	43.00				
2	.26	1.10	90	59	97	44.71				
1	.25	1.05	91	63	98	46.42				
B-12	.25	1.05	92	67	99	48.08				
11	.27	1.14	93	68	100	49.72				
10	.25	1.06	94	69	100	51.43	1			
9	.19	.81	96	71	99	53.09				
8	.17	.72	97	72	99	54.54				
7	.16	.68	98	73	99	55.90				
6	.16	.68	99	74	99	57.25	1			
5	.18	.77	100	75	99	58.64				
4	.22	.94	101	76	99	60.09				
3	.26	1.12	101	78	99	61.63				
2	.25	1.07	102	80	99	63.32	1			
1	.25	1.07	103	80	100	65.07	1	278	1125	
						66.73				

Client Name: Drax
Smithers
 Process: Dryer Stack 4
 Test Number: 2
 Date: Feb 13/25
 Start Time: 12:45
 Finish Time: 1:47
 Starting Vol.: 300
 Final Vol.: 308
 Flask: Q-6
 Console: 1039
 Stack Diameter: _____

BP 28.15
 DN .270
 CP .83829
 MF 1.0043
 Moist: _____
 PM 28.26
 AS _____
 Ko .8032
 Pitot 140
 Port _____
 Static -.16
 PS 28.15

CO ₂	O ₂	CO	N ₂
0	21		

Duct Diameters
 Up-Stream _____

Duct Diameters
 Downstream _____

Personnel: DB

Mean Yaw Angle _____

Leakage Rate @ 15 inches _____

Start: .008 Finish: .009

Load: _____

Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A-12	.27	1.15	84	84	98	66.96	0	270	1CED	
11	.28	1.20	89	86	99	68.72				
10	.24	1.03	94	87	99	70.48				
9	.22	0.95	104	88	101	72.17				
8	.17	.74	105	89	102	73.78				
7	.17	.74	106	90	102	75.16	0			
6	.16	.70	107	91	101	76.62	1			
5	.17	.74	108	92	101	78.01				
4	.22	.76	109	93	101	79.43				
3	.25	1.09	111	94	102	81.07				
2	.25	1.09	112	95	102	82.82				
1	.26	1.14	113	96	103	84.55	1			
B-12	.27	1.18	113	96	102	86.38				
11	.27	1.18	114	97	103	88.20				
10	.25	1.10	114	98	104	90.02	1			
9	.23	1.01	115	99	104	91.73				
8	.19	.83	116	100	105	93.40				
7	.18	.79	117	101	106	94.92				
6	.18	.79	118	102	106	96.41	1			
5	.17	.75	118	102	106	97.89				
4	.16	.70	119	103	107	99.33				
3	.20	.88	119	103	107	100.73				
2	.24	1.06	120	103	107	102.41				
1	.25	1.10	120	104	107	104.16	1	270	1CED	
						105.91				

Client Name: Trax
Smithers
 Process: Dryer Stack 4
 Test Number: 3
 Date: Feb 13/25
 Start Time 2:20
 Finish Time 3:22
 Starting Vol. 300
 Final Vol. 300
 Flask: Q-7
 Console: C-1039
 Stack Diameter _____

BP 28.15
 DN .270
 CP .83829
 MF 1.0043
 Moist. _____
 PM 28.26
 AS _____
 Ko .8032
 Pitot 140
 Port _____
 Static -.16
 PS 28.15

CO ₂	O ₂	CO	N ₂
0	21		

Duct Diameters
 Up-Stream _____
 Duct Diameters
 Downstream _____

Personnel: JB

Mean Yaw Angle _____

Leakage Rate @ 15-inches _____

Start: 005 Finish: 006

Load: _____


Sample Points	Delta P	Delta H	Temp. In	Temp. Out	Stack Temp.	Gas Volume	Pump Vacuum	Box Temp.	Last Imp. Temp.	Points
A-12	.26	1.07	77	81	110	6.04	0	270	iced	
11	.28	1.17	85	84	109	7.71				
10	.25	1.05	89	85	109	9.50				
9	.22	.93	90	86	109	11.20	1			
8	.18	.76	93	87	109	12.78				
7	.17	.72	94	88	109	14.22				
6	.17	.72	95	89	110	15.65				
5	.16	.68	96	90	110	17.06				
4	.23	.98	98	91	110	18.41				
3	.25	1.07	101	92	110	20.04				
2	.26	1.11	102	92	109	21.75				
1	.26	1.11	103	93	109	23.50				
B-12	.25	1.07	104	94	109	25.24				
11	.27	1.16	107	95	109	27.00	1			
10	.26	1.12	110	96	110	28.79				
9	.23	.99	111	97	110	30.55				
8	.21	.91	112	98	108	34.03				
7	.19	.83	113	99	107	35.80				
6	.16	.70	114	100	106	37.32				
5	.16	.70	114	101	105	38.75				
4	.18	.79	115	102	105	40.19	1			
3	.23	1.01	116	103	104	41.60				
2	.25	1.10	117	104	106	43.27				
1	.26	1.14	118	106	107	45.00	1	270	iced	
						46.97				




This is to verify that
Matthew McCall
has successfully completed
a course of study in
Source Testing for Particulates
(35 hours)

Endorsed by
The B.C. Ministry of Environment

Dated at Burnaby, British Columbia, Canada
December 14, 1990


DEAN


REGISTRAR

BRITISH COLUMBIA INSTITUTE OF TECHNOLOGY



MOUNT ROYAL COLLEGE

Faculty of Continuing Education and Extension

David Brandle

has successfully completed

The program of studies and is awarded the certificate in

STACK SAMPLING

May 3 – May 7, 2004

May, 2004
Date

Doreen Brandle
Dean
Faculty of Continuing Education and Extension

MOUNT ROYAL UNIVERSITY

Faculty of Continuing Education and Extension

Chris Bodden

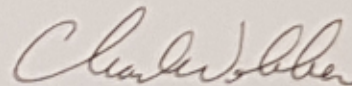
has successfully completed

Stack Sampling Seminar

35 Hours / 2017

June 23, 2017

Date



Dean

Faculty of Continuing Education and Extension



MOUNT ROYAL UNIVERSITY

Faculty of Continuing Education and Extension

Daniel Lawrence

has successfully completed

Stack Sampling
Certificate of Completion

35 Hours / 2022

October 2022

Date



Dean

Faculty of Continuing Education and Extension